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Design of a Single Stage Centrifugal Compressor as Part of a Microturbine Running at 60000 rpm, Developing a Maximum of 60 kW Electrical Power Output

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Abstract: In this current work, the design of a single stage centrifugal compressor as part of a complete small gas turbine coupled directly to high speed permanent magnet running at 60000rpm and developing a maximum electrical power of 60kW is presented. The choice of a radial impeller was considered and the design was based on using a non-linear optimisation code to determine the geometric dimensions of the impeller. Also, the optimum axial length and the flow passage of the impeller were found based on prescribed mean stream velocity. The proposed code was verified and showed quite good agreement with the published data in the open literature. The design of a vaneless diffuser and a volute were considered based on satisfying the governing equations of conservation of mass, momentum, and energy conservation simultaneously. Results showed good agreement with the CFD analysis found in the open literature. This work was motivated by the growing interest in micro-gas turbines for electrical power generation, transport and other applications.

Keywords: Centrifugal Compressor, Vaneless Diffuser, Impeller, Mean Stream Velocity, Optimization

1. Introduction

Centrifugal compressors are one of the main components of microturbines. Microturbines are gas turbines with power ranging approximately from 10 to 200kW. These devices can be used in stationary, transport and auxiliary power application. In the compressor design stage, many choices of design options need to be considered before the final design. It is essential that design engineers begin to perform a compressor design with full understanding of all aspects of the design considerations [1–4]. Many research works that have been cited in the open literature used different optimization methods such as artificial neural network (ANN) and a genetic algorithm (GA), developed computer codes, and Computational fluid mechanics (CFD) to design the centrifugal impeller. These were based on the design variables that control the shape of the impeller [5-12]. However, the superiority of these design techniques could not be validated in experimental results due to the difficulties in properly

conducting experiments.

2. Design Problems

There are many design problems when dealing with centrifugal compressors. First problem is that the flow inside the compressor is complex because the flow takes place against the positive pressure gradient; consequently it decelerates along the mean flow path. Errors in the design of the impeller, for example, may lead to excessive space rates of deceleration in the inducer section; hence produce high losses Ingham and Bhinder [13]. Second problem is the relative Mach number close to the inducer tip. In case of high-pressure ratio impellers, the inducer tip Mach number M_{er} may reach unity; consequently some part of the inlet area may be choked. Often this problem is addressed by cutting alternate blades back, resulting in splitter blades. However, it is not easy to ensure that flow rate in the resulting two channels would be equal because of the presence of jet and wake flows in the

impeller flow passages. Stahler [14] investigated the effect of inducer relative tip Mach number M_{er} on efficiency using several Boeings compressors. The results were presented indicate the penalty that may be paid for the increase in M_{er} . Efficiency falls off rapidly for M_{er} greater than 0.8.

Third problem is the radial vaneless diffuser which may be considered a major source of inefficiency in centrifugal compressors due to non-uniform flow leaving the impeller; therefore, most of the work cited in the open literature was directed to study the flow and find methods to predict the losses in the vaneless diffuser in an attempt to increase its efficiency, [15-20]. According to this, careful design is addressed to the vaneless diffuser to produce efficient compressor.

Betteni et al. [21] presented the design process for a centrifugal compressor that will be part of demonstrative micro-gas turbine plant. The design methodology developed at Dimset has been used for the fluid dynamics design of a centrifugal compressor for a small micro gas turbine plant. Zahed and Bayomi [22] presented the development of a preliminary design method for centrifugal compressors. The design process started with the aerodynamic design and its reliance on empirical rules limiting the main design parameters. This procedure can be applied to the compressors for the pressure ratios of 1.5, 3.0 and 5.0. Design considerations of mechanical stress for the impeller and minimum inlet Mach number were taken into consideration. In this research work, the authors had done the preliminary design in which the work input and compressor efficiency was considered. The impeller design at different pressure ratios has been done.

Marefat et al. [23] presented the design procedure of multi-stage centrifugal compressor, by considering one dimensional flow design. The design procedure started from calculation of impeller inlet and it is continued for the other sections including impeller exit, diffuser and volute. The total efficiency, stage efficiency, correction factors and leakages are calculated. From the procedure, it was revealed that there are essential parameters such as tip speed Mach number, flow coefficient at inlet and diameter of impeller which will play major roles in determining compressor polytropic head and consequently compressor polytropic efficiency. The designed volute is different than that the referred one. The dissimilarity rises on the grounds that the mentioned method considers minimum optimum values rather than most efficient ones, which lead to an economical design.

Kuraushi and Barbosa [24] presented the design of a centrifugal compressor for natural gas in 3 steps in which the first step has 1-D preliminary design heavily based on empirical data, the second step is the flow analysis in the meridional plane and the last step involves the CFD analysis to check if the 1-D methodology is adequate. The point of departure for the centrifugal compressor design was appropriately selected following Vavra's suggestion. Li et al. [25] presented an optimization design method for centrifugal compressors based on one dimensional calculations and

analysis. It consisted of two parts which are centrifugal compressor geometry optimization based on one dimensional calculation and match the optimization of the vaned diffuser with an impeller based on the required throat area.

Gui et al. [26] described a design and experimental effort to develop small centrifugal compressors for aircraft air cycle cooling systems and also for small vapor compression refrigeration systems. Several low-flow-rate centrifugal compressors which are featured with three-dimensional blades have been designed, manufactured and tested in this study. An experimental investigation of compressor flow characteristics and efficiency had been conducted to explore a theory for mini-centrifugal compressors. The effects of the number of blades, overall impeller configuration, and the rotational speed on compressor flow curve and efficiency were studied.

Moroz et al. [27] presented a method for centrifugal and mixed type compressor flow paths design based on a unique integrated conceptual design environment. The approach provided in the paper gives the designer the opportunity to design axial, radial and mixed flow turbo-machinery using the same tool. Bowade and Parashkar [28] presented a step by step guidance to design a radial type vane profile. In radial type vanes, the vane profile is a curve that joins the inlet and outlet diameter of the impeller which can be done in infinite number of curves and so it is required to define proper shape of the vane. In this paper, simple arc, double arc, circular arc and point by point methods were stated.

It can be concluded from previous work that there is no standard procedure of design calculations of centrifugal compressor since every engineer relies on some empirical relation. Also, published papers on complete design of centrifugal compressor as part of a complete small gas turbine coupled directly to high speed permanent magnet running at 60000rpm of 60kW power output is still scarce. Therefore, this motivated the work in this paper to present a comprehensive design of a single stage centrifugal compressor, which includes the impeller, the vaneless diffuser, and the volute as part of a microturbine for power generation running at running at 60000 rpm, and developing a maximum of 60 kW electrical power output. Furthermore, developing a design method for calculating the number of blades N_b and the axial length Z_{axial} would offer a significant contribution. In addition to that, the design of blade profile and flow channel based on prescribed mean velocity is a new approach as far as the author is aware off. The procedure of the proposed design of the centrifugal compressor is described hereafter.

PROPOSED DESIGN PROCEDURE

The design procedure of a centrifugal compressor was divided into the following two stages:

Stage (1): Firstly, the determination of the optimum geometric dimensions and number of blades of the impeller. Secondly, the optimization of axial length and passage geometry for a prescribed or assumed mean-stream velocity.

Stage (2): The design of the vaneless diffuser and the volute for which the governing equations of mass, momentum and energy equations must be satisfied simultaneously.

2.1. Impeller Design

2.1.1. Optimisation of the Principal Dimensions of the Impeller

The terminology used to define the components of a

centrifugal compressor is shown in Fig. 1 and the pressure rise across it is depicted in Fig. 2. An enthalpy – entropy diagram is plotted to show the compression process progression in the compressor stage as shown in Fig. 3.

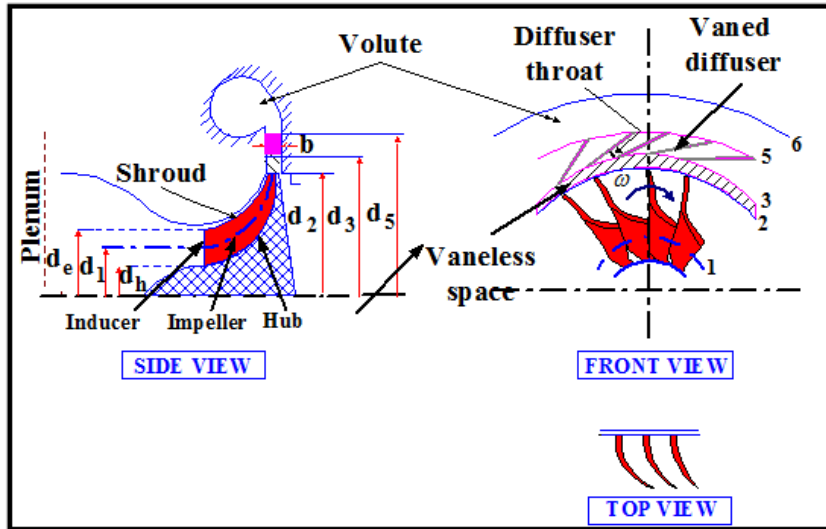


Figure 1. Components of centrifugal compressor.

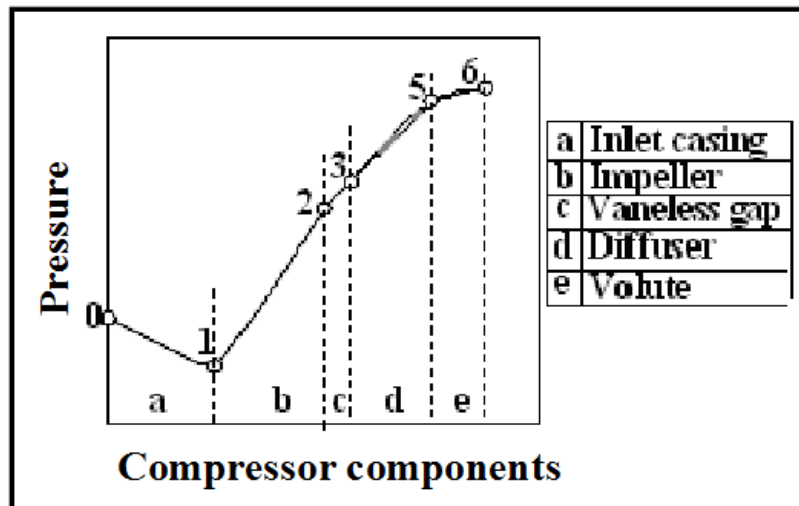


Figure 2. Pressure rise across the compressor stage.

It should be noted that the process departs from isentropic compression due to losses caused by friction, viscous drag and others. In general, the impeller of a centrifugal compressor may be considered as a generalized fluid handling system and

the variables which will completely describe the design and performance of this system may be divided into three groups as shown in Table 1.

Table 1. Main parameters of a centrifugal compressor impeller.

Control variables	Design variables	Performance requirements
Inlet pressure	Tip diameter and blade width	Mass flow rate
Inlet temperature	Inducer and hub diameters	Isentropic efficiency
Rotational speed	Axial length, blade angles	Pressure ratio
Properties of working fluids	Mach numbers	Specific speed, Diffusion ratio and Flow coefficients

$$\frac{d_e}{d_2} = \left(\frac{M_{er}}{\pi d_2 N} \right) \left[\frac{(\gamma-1) \cos^2 \beta_e}{1 + \frac{\gamma-1}{2} M_{er}^2 \sin^2 \beta_e} \right] \quad (5)$$

$$\frac{d_h}{d_2} = \left(\frac{d_e}{d_2} \right) \sqrt{1 - \frac{\left(\frac{\dot{m} \sqrt{C_{pa} T_{01}}}{d_2^2 P_{01}} \right) \left\{ 1 + \frac{\gamma-1}{2} (M_{er} \sin \beta_e)^2 \right\}^{\frac{\gamma+1}{2(\gamma-1)}}}{(B_{f1}) \left(\frac{\pi}{4} \right) \left(\frac{\gamma}{\sqrt{\gamma-1}} \right) \left(\frac{d_e}{d_2} \right)^2 (M_{er} \sin \beta_e)}} \quad (6)$$

Where:

$$\frac{b_2}{d_2} = \left(\frac{1}{\pi^2 \phi_s B_{f2}} \right) \left(\frac{\gamma-1}{\gamma} \right) \left[\frac{\left(\frac{\dot{m} \sqrt{C_{pa} T_{01}}}{d_2^2 P_{01}} \right) \left(1 + \frac{1}{\eta_c} \left(\frac{P_{02}}{P_{01}} \right)^{\gamma-1/\gamma} - 1 \right)}{\left(\frac{P_{02}}{P_{01}} \right) \left(\frac{d_2 N}{\sqrt{C_{pa} T_{01}}} \right) (\tan \alpha_2)} \right] \times \left[1 - 0.5 \left(\frac{\pi \phi_s}{\cos \alpha_2} \right)^2 \left\{ \frac{\left(\frac{d_2 N}{\sqrt{C_{pa} T_{01}}} \right)^2}{1 + \frac{1}{\eta_{cc}} \left\{ \left(\frac{P_{02}}{P_{01}} \right)^{\frac{\gamma-1}{\gamma}} - 1 \right\}} \right\} \right]^{\frac{-1}{(\gamma-1)}} \quad (8)$$

Where:

$$B_{f2} = 1 - \frac{1}{\pi} \left[n \left(\frac{\bar{t}_2}{d_2} \right) \right]$$

2.1.2. Optimization Procedure

For a given set of design conditions as listed in Table 2, the optimum geometric dimensions of the impeller were found by solving Eqns. (1) to (8) within the specified ranges of the constraints variables. The solution can be obtained by using a suitable optimisation algorithm. In view of this, numerical optimisation techniques can be a useful tool to problems involving a large number of variables.

Table 2. Compressor input data at design point.

Design Variables	Design Values
Mass flow, \dot{m}_a	0.566
Pressure ratio, P_{02}/P_{01}	4/1
Inlet stagnation temperature, T_{01}	300° K
Rotational speed, N	60,000 rpm
Average blade thickness at impeller inlet, \bar{t}_{th2}	2.0 mm
Average blade thickness at impeller outlet, \bar{t}_{th1}	2.0 mm

The authors used the algorithms called optimisation using recursive quadratic programming OPRQP developed by Biggs [29, 30]. The optimisation programme started by assigning different values to a set of parameters $X_1, X_2, X_3, \dots, X_n$. Therefore, an objective function denoted by $F(\bar{X})$, where \bar{X} is a vector with elements, $X_1, X_2, X_3, \dots, X_n$ must be formulated and the aim is to determine the values of the vector \bar{X} , which will find the optimum value of the function $F(\bar{X})$. This function may be subjected to possible

$$B_{f1} = \frac{2}{\pi} \frac{n(\bar{t}_{th1}/d_2)}{\left[(d_e/d_2) + (d_h/d_2) \right]}$$

(ii). Impeller Outlet Design Parameters

a. Diffusion ratio parameter (v_2/v_1)

$$\frac{v_2}{v_1} = \pi(1-\phi_s) \left(\frac{\sin \beta_1}{\cos \beta_2} \right) \left(\frac{\sqrt{\frac{1}{\gamma-1} + \frac{M_{er}^2 \sin^2 \beta_e}{2}}}{M_{er} \sin \beta_e} \right) \left(\frac{1}{\pi} \sqrt{\frac{1}{\eta_c} \left(\frac{P_{02}}{P_{01}} \right)^{\gamma-1/\gamma} - 1} \right) \quad (7)$$

b. Blade tip width to impeller tip diameter ratio expression (b_2/d_2)

linear or non- linear equality and inequality constraints, i.e.

$$g_i(\bar{x}) = 0 \quad i = 1, \dots, q \quad (9)$$

$$g_j(\bar{x}) \geq 0 \quad j = q+1, \dots, m \quad (10)$$

Where: g_i and g_j represent non-linear equality and inequality constraints, respectively. The subscripts i and j refer to the number of constraints.

(i). Constraint Optimisation Technique Procedure

The frame size and weight of centrifugal compressor is often an important parameter consideration, in view of this, the size of the impeller plays an important rule in determining the overall size of such a compressor. Therefore, the aim is to minimise the impeller tip diameter d_2 and this can be considered a constraint optimisation problem. The procedure to solve such a problem is described below:

a. Selection of main principal parameters of a turbine rotor

The choice of selecting the principal parameters of a compressor impeller to solve this optimisation problem is given by the matrix:

$$\bar{X} = \begin{bmatrix} d_2 = X(1) \\ M_{er} = X(2) \\ \beta_e = X(3) \\ d_e/d_2 = X(4) \\ d_h/d_2 = X(5) \\ \alpha_2 = X(6) \\ b_2 = X(7) \\ v_2/v_1 = X(8) \\ \beta_2 = X(9) \\ M_2 = X(10) \\ \beta_1 = X(11) \end{bmatrix} \quad (11)$$

b. Formulation of the objective function

The objective function is to optimise the rotor tip diameter and it can be formulated as follows:

Minimize

$$F(\bar{X}) = d_2 = X(1) \quad (12)$$

$$g(1) = \frac{\dot{m}\sqrt{C_{pa}T_{01}}}{d_2^2 P_{01}} - \left(\frac{\gamma}{\sqrt{\gamma-1}}\right) \left[B_{f_1} \left(\frac{\pi}{4}\right) \left(\frac{d_e}{d_2}\right)^2 - \left(\frac{d_h}{d_2}\right)^2 \right] \left[\frac{M_{er} \sin \beta_e}{\left(1 + \frac{\gamma-1}{2} (M_{er} \sin \beta_e)^2\right)^{\gamma/2(\gamma-1)}} \right] \quad (13)$$

a.2

$$g(2) = \frac{b_2}{d_2} - \left(\frac{1}{\pi B_{f_2}}\right) \left(\frac{\sqrt{\gamma-1}}{\gamma}\right) \left[\frac{\left(\frac{\dot{m}\sqrt{C_{pa}T_{01}}}{d_2^2 P_{01}}\right) \left(1 + \frac{1}{\eta_c} \left(\frac{P_{02}}{P_{01}}\right)^{\gamma-1/\gamma} - 1\right)^{1/2}}{\left(\frac{P_{02}}{P_{01}}\right)} \right] \left[\frac{\left(1 + \frac{\gamma-1}{2} M_2^2\right)^{\frac{\gamma+1}{2(\gamma-1)}}}{M_2 \sin \alpha_2} \right] \quad (14)$$

a.3

$$g(3) = \frac{v_2}{v_1} - \pi(1 - \varphi_{sf}) \left(\frac{\sin \beta_1}{\cos \beta_2}\right) \left(\frac{\sqrt{\frac{1}{\gamma-1} + \frac{M_{er}^2 \sin^2 \beta_e}{2}}}{M_{er} \sin \beta_e}\right) \left(\frac{1}{\pi} \sqrt{\frac{1}{\eta_c} \left(\frac{P_{02}}{P_{01}}\right)^{\gamma-1/\gamma} - 1}\right) \quad (15)$$

a.4

$$g(4) = \frac{b_2}{d_2} - \left(\frac{N_b}{234.4}\right) \left(\frac{1/\varphi_{sf} - 1}{\tan \alpha_2}\right) \quad (16)$$

b.6 $\alpha_2 \geq 17^\circ$: Controlled by diffusion ratio

$$g(10) = \alpha_2 - 17^\circ \quad (22)$$

b. Inequality constraints

b.1 $d_2 \leq 20.0 \text{ cm}$: This is governed by the size of the compressor

$$g(5) = 20.0 - d_2 \quad (17)$$

b.7 $b_2 \geq 0.004$: Governed by leakage loss and diffusion ratio

$$g(11) = b_2 - 0.004 \quad (23)$$

b.2 $M_{er} \leq 1.0$: Specified by the subsonic flow requirements

$$g(6) = 1.0 - M_{er} \quad (18)$$

b.8 $v_2/v_1 \geq 0.55$: Governed by flow separation in the impeller passage

$$g(12) = v_2/v_1 - 0.55 \quad (24)$$

b.3 $\beta_e \geq 25^\circ$: Specified by maximum flow at inducer inlet

$$g(7) = \beta_e - 25^\circ \quad (19)$$

b.9 $\beta_2 \geq 60^\circ$: Specified by diffusion ratio requirements

$$g(13) = \beta_2 - 60^\circ \quad (25)$$

b.4 $d_e/d_2 \geq 0.55$: Governed by the relative Mach number

$$g(8) = d_e/d_2 - 0.55 \quad (20)$$

b.10 $M_2 \geq 0.95$: fixed by relative flow angle at impeller exit

$$g(14) = M_2 - 0.95 \quad (26)$$

b.5 $d_h/d_2 \leq 0.40$: Specified by stress limitation and number of blades.

$$g(9) = 0.40 - d_h/d_2 \quad (21)$$

b.11 $\beta_1 \geq 35^\circ$: Governed by inducer and hub diameter

$$g(15) = \beta_1 - 35^\circ \quad (27)$$

(ii). **Optimisation Programme**

The optimisation using recursive quadratic programming Fortran programme, double precision, OPRQP is used to solve

a general non-linear programming problem using the successive quadratic programming algorithm and a user-supplied gradient. The description of the OPRQP programme is found in Refs. [29-31]. The only unusual feature is the use of the impeller tip diameter d_2 as an optimisation variable and an objective function. However, such a choice should not affect the working of the programme. The objective function and the equality and inequality constraints with their first derivatives are inserted into the programme into two sub-routines called, call function and call gradient.

2.1.3. Optimisation Results

The optimisation program was run for a number of blades ranging from 12 to 20. The number of blades was specified within this range in accordance with the assumed efficiency η_c , blockage B_f and blade loading factor C_{w2}/u_2 . Fig. 5 shows the impeller tip diameter d_2 and the impeller tip width b_2 plotted against the number of blades N_b . As one would expect, the tip width increases as the diameter is reduced for the blade number from 12 to 15, then the change for both d_2 and b_2 is fairly small. The design outlet and inlet velocity diagrams based on optimisation technique are shown in Fig. 6a and 6b. Also, the complete results of the design are given in Table 3a and 3b, respectively.

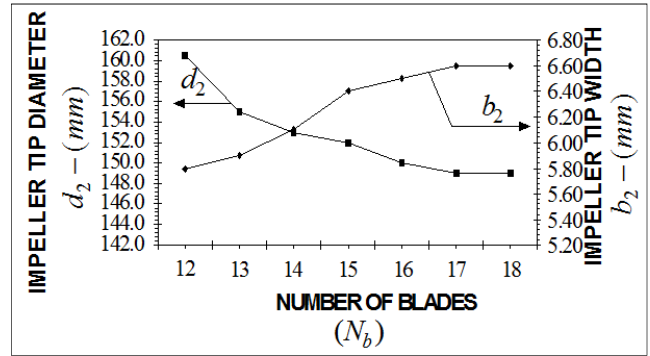


Figure 5. Plot of impeller tip diameter and tip width against The number of blades.

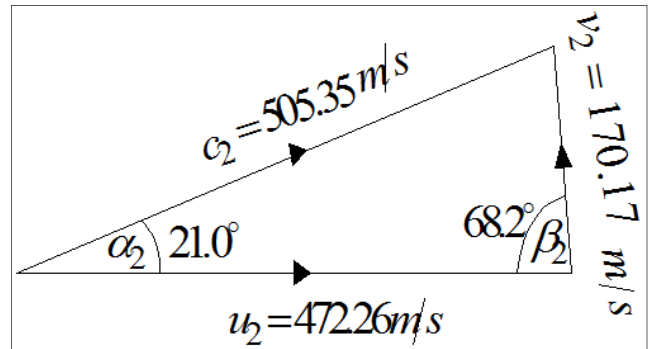


Figure 6a. Outlet velocity triangle based on numerical optimization technique.

Table 3a. Results data (1) for the impeller based on numerical optimization.

Design Parameters	Geometrical Dimensions	Flow Angles at Impeller Inlet and Exit	Performance Parameters
$\dot{m}_a = 0.566 \text{ kg/s}$	$d_2 = 15.19 \text{ cm}$	$\alpha_2 = 21.0^\circ$	$S_p = 0.277$
$N = 60000 \text{ rpm}$	$b_2 = 0.64 \text{ cm}$	$\beta_2 = 68^\circ$	
$\frac{P_{02}}{P_{01}} = 4.0$	$\bar{t}_{th2} = 0.2 \text{ cm}$	$\alpha_1 = 90^\circ$	$M_p = 0.134$
$T_{01} = 300 \text{ K}$	$d_1 = 6.387 \text{ cm}$	$\alpha_h = 90^\circ$	$\eta_c = 0.83$
$t_1 = 288.16 \text{ K}$	$d_h = 3.038 \text{ cm}$	$\alpha_e = 90^\circ$	$c_{m1}/u_2 = 0.33$
$p_1 = 0.87 \text{ bar}$	$d_e = 8.506 \text{ cm}$	$\beta_h = 58.53^\circ$	$v_2/v_1 = 0.67$
$\rho_1 = 1.05 \text{ kg/m}^3$	$\bar{t}_{th1} = 0.2 \text{ cm}$	$\beta_1 = 37.56^\circ$	
		$\beta_e = 30^\circ$	

Table 3b. Results data (2) for the Impeller based on numerical optimization.

Flow Velocities at Impeller Exit	Flow Velocities at Impeller Inlet	Blade Speed at Impeller Inlet and Outlet	Mach Number at Impeller Inlet and Exit
$c_2 = 505.35 \text{ m/s}$	$c_1 = 154.29 \text{ m/s}$		$M_2 = 1.14$
$c_{m2} = 158.28 \text{ m/s}$	$c_{w1} = 0.0 \text{ m/s}$	$u_2 = 476.27 \text{ m/s}$	$M_{r2} = 0.65$
$c_{w2} = 412.32 \text{ m/s}$	$c_h = 154.29 \text{ m/s}$	$u_1 = 292.18 \text{ m/s}$	$M_1 = 0.453$
$v_2 = 170.71 \text{ m/s}$	$c_e = 154.29 \text{ m/s}$	$u_h = 95.18 \text{ m/s}$	$M_{hr} = 0.532$
$v_{m2} = 158.28 \text{ m/s}$	$v_1 = 253.10 \text{ m/s}$	$u_e = 276.24 \text{ m/s}$	$M_{1r} = 0.743$
$v_{w2} = 63.95 \text{ m/s}$	$v_{w1} = 200.65 \text{ m/s}$		$M_{er} = 0.903$
	$v_h = 180.89 \text{ m/s}$		
	$v_e = 308.58 \text{ m/s}$		

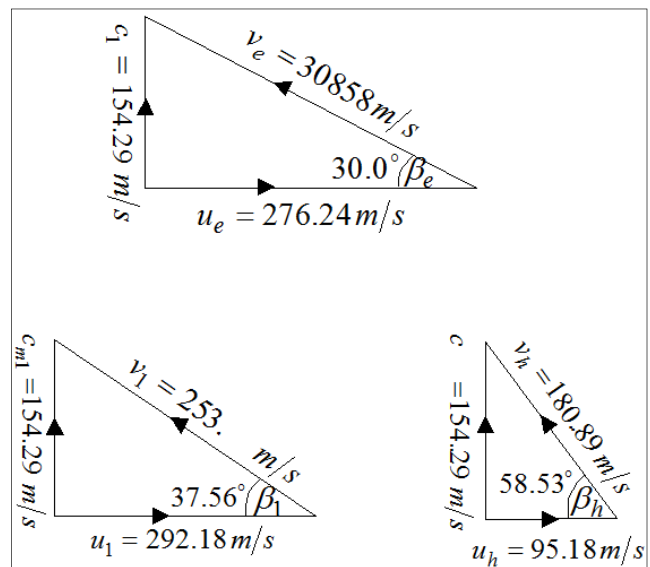


Figure 6b. Inlet velocity triangle based on numerical optimization technique.

2.2. Optimization of Passage Geometry and the Choice of Axial Length

To define the passage geometry of the impeller, the axial length of the impeller is almost a pre-requisite. Therefore, a prescribed mean stream velocity distribution approach was used to optimize the passage geometry and the axial length of the impeller.

The relative velocity vector \vec{V} at any point inside the

impeller passage, as shown in Fig. 7, can be resolved into three basic components along the axial, radial and tangential directions, \vec{V}_z , \vec{V}_r and \vec{V}_w , Here \vec{V}_m is the velocity vector along the mean streamline in the hub-to-shroud plane, hence

$$\vec{V} = \vec{V}_z + \vec{V}_r + \vec{V}_w \quad (28)$$

The boundary values of the components of the relative velocity are known from the inlet and outlet velocity triangles, which resulted from the previous optimisation. These boundary values are given as follows:

At impeller inlet:

$$V_z = (V_z)_{\max}, \quad V_r = 0$$

At impeller exit:

$$V_z = 0, \quad V_r = (V_r)_{\max}, \quad \text{and} \quad V_w = (1 - C_{w2}/U_2)U_2$$

From Fig. 7, the following relations are hold

$$V = V_z + V_r + V_w, \quad V = V_w + V_m \quad (29)$$

and

$$V_m = V_r + V_z, \quad V_w = V \sin \beta, \quad V_r = V_m \sin \alpha, \quad V_z = V_m \cos \alpha,$$

$$\beta = \sin^{-1} \sqrt{1 - V_m^2 / V^2} \quad (30)$$

The angles shown in Fig. 7 above can be expressed in terms of the velocities as shown:

But, $\tan \beta = \frac{V_w}{V_m}$, $\tan \theta = \frac{V_w}{V_z}$, and $\cos \alpha = \frac{V_z}{V_m}$

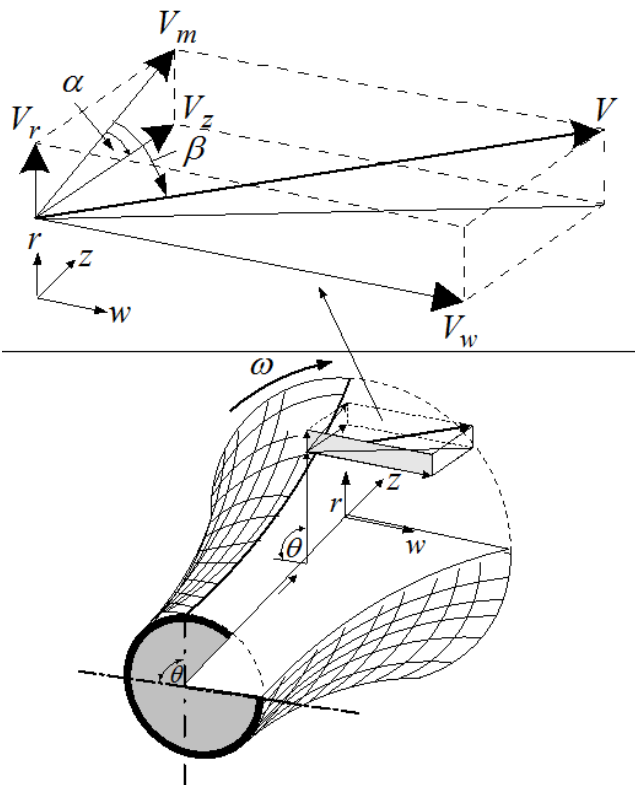


Figure 7. Schematic for the relative velocity vector and its components.

The angles (α , β and θ) are related to each other by combining the above relationships as follows:

$$\tan \beta = \tan \theta \cos \alpha \quad (31)$$

The spatial description of the mean streamline can be found iteratively by assuming a starting value for the meridional length z_m , and the distributions of the relative velocity vector.

Figure 8 describes the velocity components V_r , V_z and V_w for one assumed value of $Z = 0.06 m$. At the start, all these figures are based on the assumption that the variation of the relative velocity vector V is linear. A computer program was written to perform the iterative calculations to check this linear relationship variation of relative velocity vectors along the mean streamline and the flow angles α and β . The output results are plotted in Fig. 9 and 10, and a flow chart based on this program is shown in Fig. 11.

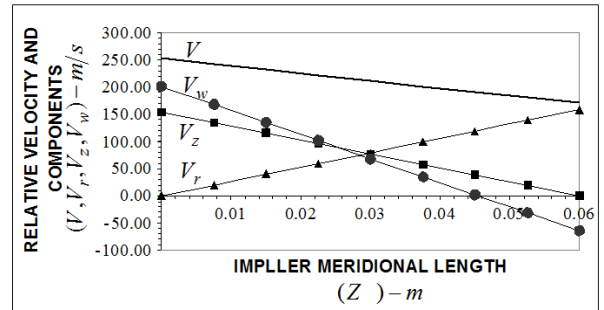


Figure 8. Assumed linear relationship of relative velocity vector mean and its components for an assumed $Z = 0.06 m$.

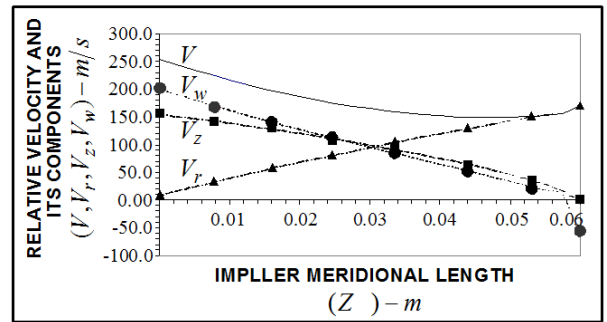


Figure 9. Prescribed relative velocity distribution along streamline for an assumed meridional length of $z_m = 0.06 m$.

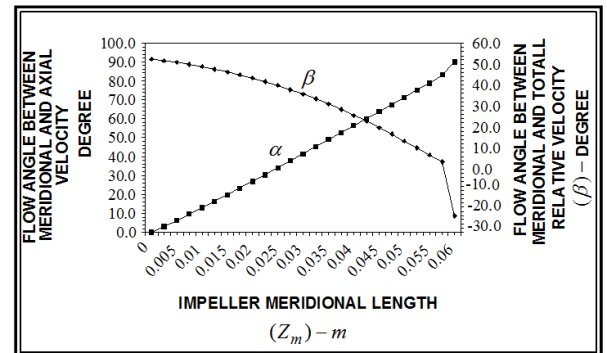


Figure 10. Actual values of the flow angles α and β along mean streamline of a meridional length of $z_m = 0.06 m$

2.3. Loss Models

Several models are available in the published literature Dallenbach [32] and Rodgers [33] which takes account of the losses. These loss models were adopted for the impeller as given in Eqns. 32 and 33, respectively. A detailed review and derivation of these loss models are outside the scope of this paper, but it should be mentioned that any loss models might be integrated into the program as sub-routine.

2.3.1. Skin Friction Loss

Skin friction loss expression at any section X as a dimensionless quantity is given by:

$$[(\Delta q)_{SFL}]_x = (0.4424) \left[(R_e)^{-1/4} \left\{ R_e \left(\frac{b_{av}}{r_c} \right)^2 \right\}^{1/20} \right] \left(\frac{\Delta l}{d_{hydr}} \right)_x \left(\frac{V^2}{u^2} \right)_x \quad (32)$$

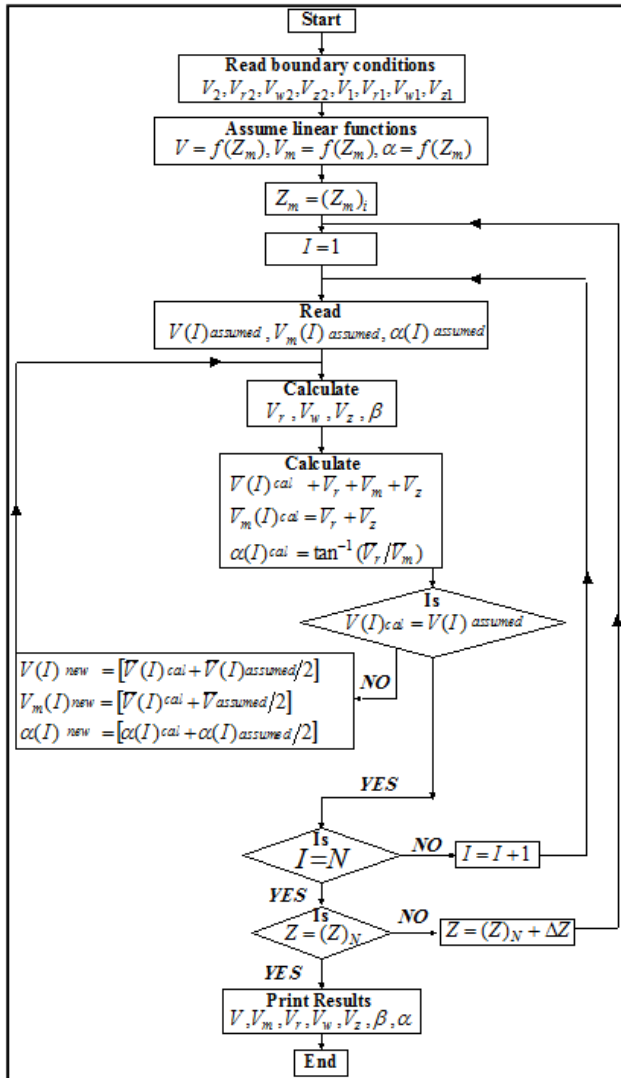


Figure 11. Flow chart for relative velocity vector variation along mean streamline.

2.3.2. Combined Diffusion and Blade Loading Losses

Combined diffusion and blade loading losses expression at any section X as a dimensionless quantity is given as:

$$[(\Delta q)_{DBL}]_x = 0.05 \left[1 - \left(\frac{v_x}{v_1} \right) \left(1 + \frac{\pi d \sin \beta}{2 \Delta l} \right)_x + \left(\frac{\pi d u}{2 \Delta l v_1} \right)_x \right]^2 \quad (33)$$

2.3.3. Shock Losses

These losses are ignored as the flow is subsonic. The next step was to optimize the axial length Z by minimizing the loss of stagnation pressure in the flow channels. Therefore, a computer program was written to optimize the axial length and the flow passage based on the relations listed here. Here the radius r of the mean streamline in the meridional plane can be represented using Lamé' ovals relationship as:

$$r = (r - r_2) \left[1 - \left(\frac{z_m - z_{m1}}{z_{m2} - z_{m1}} \right)^3 \right]^{1/2} + r_2 \quad (34)$$

The first and second derivatives of dr/dz are given in Eqns. 35 and 36, respectively:

$$\frac{dr}{dz} = - \left[\frac{3}{2} \right] \left(\frac{r_1 - r_2}{z_{m2} - z_{m1}} \right) \frac{l}{j} \left(\frac{z_m - z_{m1}}{z_{m2} - z_{m1}} \right)^2 \left(\frac{r - r_2}{r_1 - r_2} \right)^{-1} \quad (35)$$

$$\frac{d^2 r}{dz_m^2} = \left[\frac{dr}{dz_m} \right] \left[\left(\frac{2}{z_m - z_{m1}} \right) + \left(\frac{-1}{r - r_2} \right) \left(\frac{dr}{dz_m} \right) \right] \quad (36)$$

The length of the streamline is given by:

$$L = \int_{z_{m1}}^{z_{m2}} \left(1 + \left(\frac{dr}{dz_m} \right)^2 \right)^{1/2} dz_m \quad (37)$$

The temperature at any section X inside the passage

$$T_x = T_{01} \left(1 + \frac{u_x^2}{2 C_{pa} T_{01}} \right) \quad (38)$$

The pressure at any section X inside the passage

$$\frac{P_x}{\phi P_{01}} = \left(\frac{T_x}{T_{01}} \right)^{\gamma/\gamma-1} \quad (39)$$

The density at any section inside the passage

$$\rho_x = \left(1 - \frac{v_x^2}{2 C_p T_x} \right)^{1/\gamma-1} \left(\frac{P_x}{RT_x} \right) \quad (40)$$

The shroud contours at any section X inside the passage

$$r_{sx} = \sqrt{(r_{rms}^2)_x + \frac{1}{2} \frac{\dot{m}_a \cos \alpha_x}{\pi \rho_x v_{mx} B_{fx}}} \quad (41)$$

The hub contours at any section X inside the passage

$$r_{hx} = \sqrt{(2r_{rms}^2)_x - r_{sx}^2} \quad (42)$$

It can be seen from Eqns. 27 and 28 that they can be used to calculate the shroud and the hub contours at any section X inside the blade passage, hence the final shape of the blade passage can be defined. A flow diagram for optimising the axial length and flow passage of the impeller is given in Fig. 12. The output results are presented graphically. Fig. 13 shows a plot of impeller internal losses, that is, skin friction losses Δq_{SFL} and diffusion and blading losses Δq_{DBL} vs. meridional length of a centrifugal impeller. As one would expect that Δq_{SFL} is lowest for the smallest axial length and increases as the axial length is increased while Δq_{DBL} is highest for the smallest axial length and decreases as the axial length is increased. Figure 14 shows a plot of total pressure loss inside the passage vs. meridional length of a centrifugal impeller. It can be seen that the optimum meridional length was found to be 41.5 mm for minimum pressure loss in the passage.

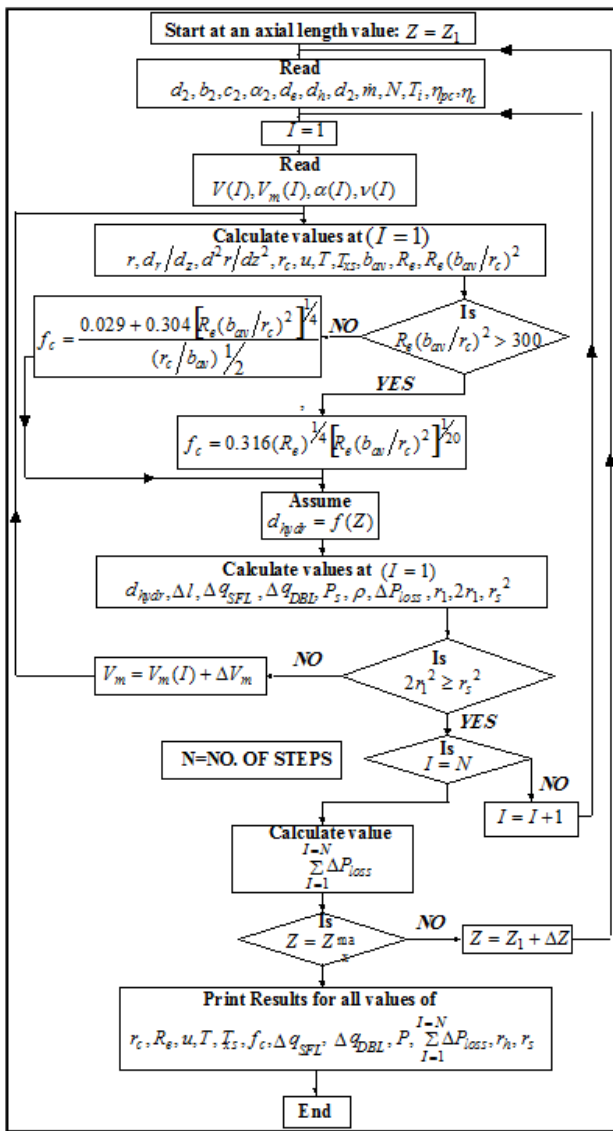


Figure 12. Flow chart for the design of the flow passage and optimization of the meridional length.

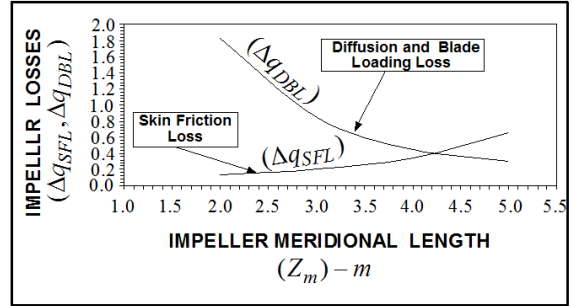


Figure 13. Variations of impeller internal losses along the impeller passage.

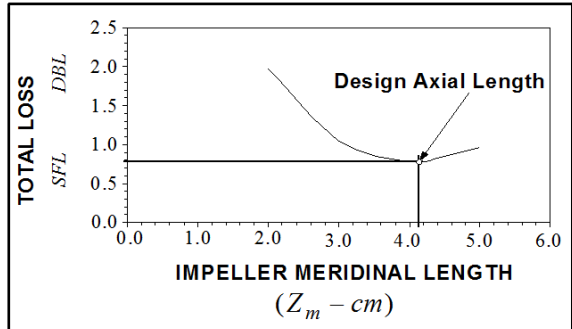


Figure 14. Overall impeller internal losses along the impeller passage.



Figure 15. Three dimensional solid model of the designed impeller.

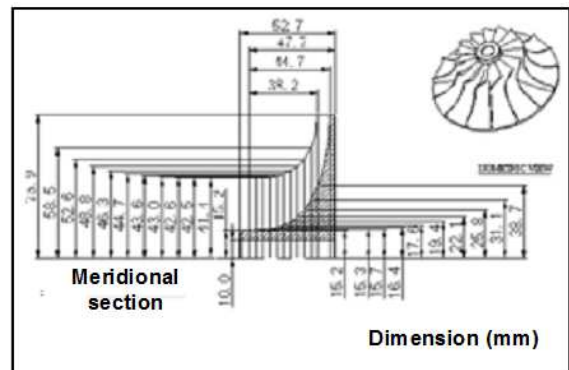


Figure 16. Detail design drawing of meridional section of the designed impeller.

2.4. Validation of the Optimization Code

The aim of this validation is to check the reliability of present code to be used with confidence for the flow analysis. The data published by Eckardt [34] and Tough et al. [35] were chosen to validate the present code. Eckardt [34] performed measurements for detailed investigation of flow field in a centrifugal impeller. The measured data have been widely used to validate computational codes and also quoted

in describing the flow characteristics along the impeller. Tough et al. [35] carried out a CFD analysis to determine the solution of the flow of a centrifugal impeller. Results of present calculations of the geometric parameters in this work show quite good agreement with the published work in the open literature [34, 35]. The discrepancies between the results can be attributed to the different input parameters of the impellers as shown in Table 5.

Table 4. Geometric parameters of Eckardt impeller and Tough et al. [35].

Parameter	Proposed impeller	Tough et al. [35] Impeller (CFD analysis)	Eckardt [34] impeller (computational code)
Inlet tip diameter	$d_t = 8.506\text{ cm}$	$d_t = 5.48\text{ cm}$	$d_t = 28\text{ cm}$
Inlet hub diameter	$d_h = 3.038\text{ cm}$	$d_h = 2.87\text{ cm}$	$d_h = 9.0\text{ cm}$
Outlet diameter	$d_o = 15.9\text{ cm}$	$d_o = 9.52\text{ cm}$	$d_o = 20\text{ cm}$
Impeller exit width	$b_2 = 0.64\text{ cm}$	$b_2 = 0.32\text{ cm}$	$b_2 = 2.6\text{ cm}$
Inlet blade angle	$\beta_1 = 37.6^\circ$	$\beta_1 = 30.0^\circ$	$\beta_1 = 30.0^\circ$
Pressure ratio	$P_r = 4.0$	$P_r = 4.2$	$P_r = 4.3$
Mass flow rate	$\dot{m} = 0.566\text{ kg/s}$	$\dot{m} = 1.45\text{ kg/s}$	$\dot{m} = 5.31\text{ kg/s}$
Inlet total temperature	300° K	288° K	288° K

Table 5. Comparison of results between the proposed impeller with Eckardt [34] and Tough et al. [35] impellers.

Parameter	Proposed impeller	Tough et al. [35] impeller	Eckardt impeller [34]
	Numerical results	CFD results	Measured results
Inlet absolute velocity	$c_1 = 154.29\text{ m/s}$	$c_1 = 136.30\text{ m/s}$	$c_1 = 135.90\text{ m/s}$
outlet absolute velocity	$c_2 = 505.35\text{ m/s}$	$c_2 = 403.90\text{ m/s}$	$c_2 = 470.74$
Inlet relative velocity	$v_1 = 253.10\text{ m/s}$	$v_1 = 268.50\text{ m/s}$	$v_1 = 263..20\text{ m/s}$
Outlet relative velocity	$v_2 = 170.71\text{ m/s}$	$v_2 = 175.40\text{ m/s}$	$v_2 = 180.25\text{ m/s}$
Inlet relative Mach number	$M_{r1} = 0.743$	$M_{r1} = 0.797$	$M_{r1} = 0.78$
Outlet relative Mach number	$M_{r2} = 0.65$	$M_{r2} = 0.61$	$M_{r2} = 0.60$

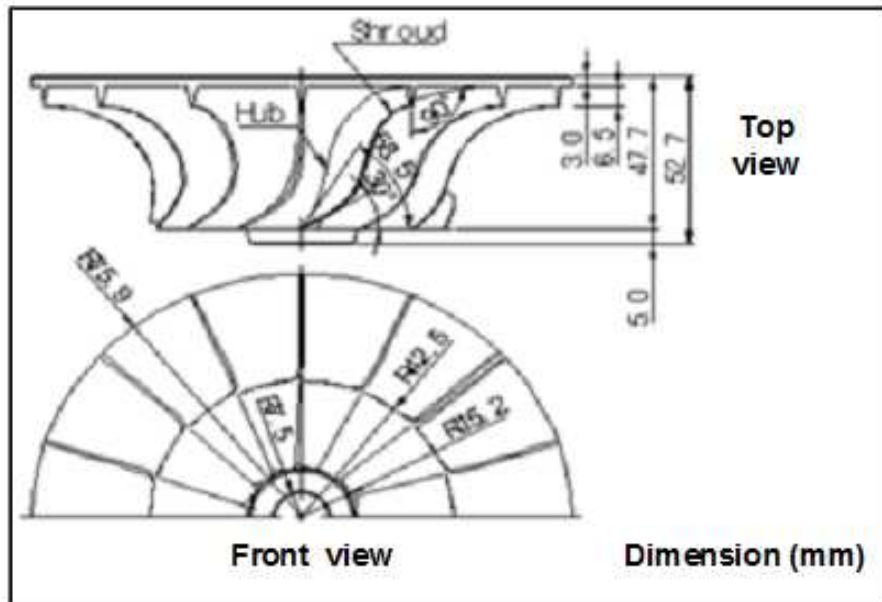


Figure 17. Detail design drawing of the designed impeller.

3. Vaneless Diffuser

The vaneless diffuser is often adopted as the sole means of pressure recovery owing to its simplicity and inexpensive construction, its broad operating range and its ability to reduce

a sonic absolute velocity to a subsonic one without the formation of shock waves. Vaneless diffusers are very common in automotive turbochargers and refrigeration compressors. They have been used in certain important applications where the impeller exit kinetic energy is too great for satisfactory volute performance and where vaned diffuser

is unsatisfactory. The vaneless diffuser may be a vaneless space between the impeller tip and the beginning of a channel or cascade diffuser or it may be run from the impeller discharge to the volute inlet. Analysis in the previous section showed that the fluid discharges from the impeller at high velocity, see Table 3, and consequently it is essential to convert the kinetic energy efficiently into static pressure. The vaneless diffuser considered in the current paper is two parallel walls forming an open passage from the impeller tip to a specified discharge diameter as shown in Fig. 18. The following section describes the design procedure.

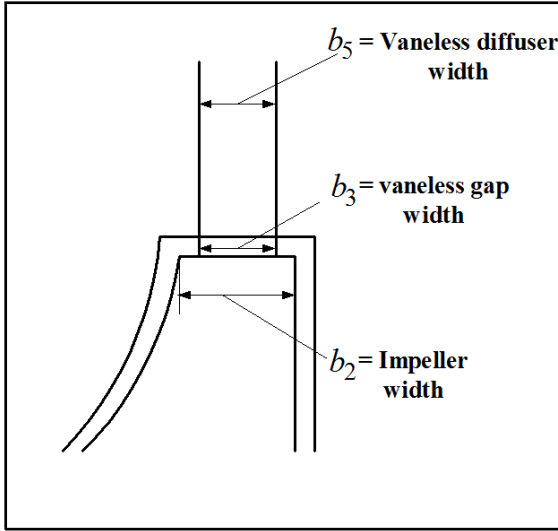


Figure 18. Reduced width in vaneless gap of a centrifugal compressor casing.

Vaneless Diffuser Design Analysis

The flow at entry to the vaneless diffuser is extremely complex, consisting of jet and wakes issuing from each passage of the impeller Dean and Senoo [19]. Therefore, mixing out occurs as the flow leaves the impeller tip at a finite radial increment outside impeller known as the vaneless gap where the flow is exposed to sudden enlargement forming eddies and friction losses. Fisher [36] gives a diameter ratio of the vaneless gap to the impeller tip d_3/d_2 is equal to 1.1 to reduce non-uniformity and noise. The simplest description of the flow through the vaneless diffuser can be obtained by considering the angular momentum equation used for the impeller but applied between the impeller exit (2) and the vaneless diffuser exit (5), (refer to Fig. 2), that is

$$\tau = \dot{m}(c_{\omega 5}r_5 - c_{\omega 2}r_2) \quad (43)$$

For the case of an open passage where the flow is only retained by the side walls and in the absence of any wall friction force, the torque τ exerted on the fluid is zero and the angular momentum equation above reduces to free vortex relationship

$$c_{\omega 5}r_5 = c_{\omega 2}r_2 \quad (44)$$

At any station along the diffuser in relation to impeller exit, the above equation is written as:

$$c_{\omega}r = c_{\omega 2}r_2 \text{ or } c_{\omega}d = c_{\omega 2}d_2 \quad (45)$$

Applying mass continuity at any station along the diffuser in relation to impeller exit would give:

$$\dot{m} = \rho_2 A_2 c_{m2} = \rho A c_m$$

$$\dot{m} = \rho_2 A_2 c_{\omega 2} \tan \alpha_2 = \rho A c_{\omega} \tan \alpha \quad (46)$$

Combining equations 45 and 46 with the equation of state $p = \rho RT$ and substituting for $\frac{A_2}{A} = \frac{\pi b_2 d_2}{\pi db}$ and re-arranging would give an expression for static pressure ratio in the vaneless diffuser:

$$\frac{p}{p_2} = \left(\frac{t}{t_2}\right) \left(\frac{b_2}{b}\right) \left(\frac{\tan \alpha_2}{\tan \alpha}\right) \quad (47)$$

For adiabatic condition in the vaneless diffuser, temperature ratio in the vaneless diffuser can be expressed as:

$$\frac{t}{t_2} = \frac{1 - \frac{c^2}{2C_{pa}T_{02}}}{1 - \frac{c_2^2}{2C_{pa}T_{02}}} \quad (48)$$

and from general velocity triangle, the velocities c and c_2 can be expressed as

$$c = \frac{c_{\omega}}{\cos \alpha} = \frac{c_{\omega 2}(r_2/r)}{\cos \alpha} \text{ and } c_2 = \frac{c_{\omega 2}}{\cos \alpha_2} \quad (49)$$

Substituting for c_2 and c expressions in Eqn. 49 and combining with Eqns. 47 and 48 will give an expression for static pressure rise ratio within the vaneless diffuser as:

$$\frac{p}{p_2} = \left[\frac{1 - \frac{\left(\frac{c_{\omega 2}}{\cos \alpha}\right)^2 \left(\frac{r_2}{r}\right)^2}{2C_{pa}T_{02}}}{1 - \frac{\left(\frac{c_{\omega 2}}{\cos \alpha_2}\right)^2}{2C_{pa}T_{02}}} \right] \left[\frac{b_2}{b} \right] \left[\frac{\tan \alpha_2}{\tan \alpha} \right] \quad (50)$$

For parallel wall vaneless diffuser, the width $b = b_3 = b_5$, hence Eqn. 50 becomes:

$$\frac{p}{p_2} = \left[\frac{1 - \frac{\left(\frac{c_{\omega 2}}{\cos \alpha}\right)^2 \left(\frac{r_2}{r}\right)^2}{2C_{pa}T_{02}}}{1 - \frac{\left(\frac{c_{\omega 2}}{\cos \alpha_2}\right)^2}{2C_{pa}T_{02}}} \right] \left[\frac{b_2}{b_5} \right] \left[\frac{\tan \alpha_2}{\tan \alpha} \right] \quad (51)$$

Equation 51 showed that the static pressure rise in the

vaneless diffuser is a function of radius ratio r/r_2 and the absolute flow angle α . For an efficient diffusion, the flow angle α must be reduced with increasing radius ratio. Eqn. 51 is plotted as shown in Fig. 19 to show the variation of pressure recovery in the vaneless diffuser. Figure 20 shows the variation of both the tangential and radial velocities with radius ratio in the vaneless diffuser. It can be seen that both velocities are decreasing with increasing radius ratio. The final design data of the vaneless diffuser parameters at exit are given in Table 6.

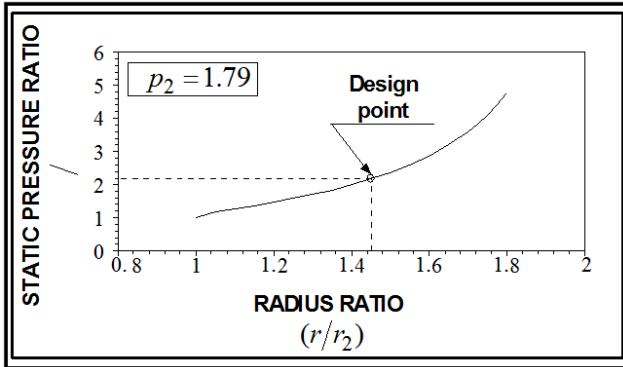


Figure 19. Pressure rise in the vaneless diffuser.

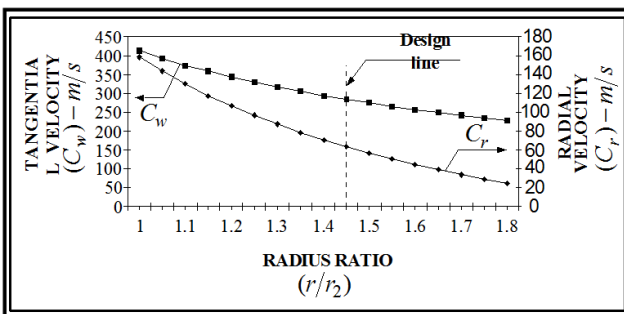


Figure 20. Variation of tangential and radial velocities with radius in the vaneless diffuser.

The final design drawing of the vaneless diffuser is shown in Fig. 21 and a three-dimensional solid model of the vaneless diffuser is shown in Fig. 22.

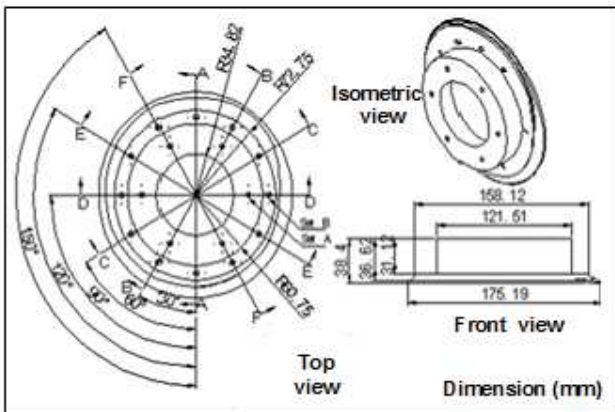


Figure 21. Detail design drawing of the vaneless diffuser.

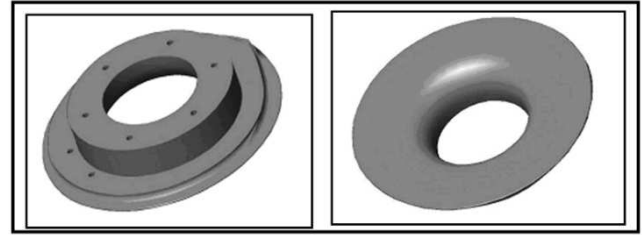


Figure 22. Three dimensional solid model of the vaneless diffuser.

Table 6. Complete design data of vaneless diffuser.

Design parameters	Design values
Vaneless diffuser diameter, d_5	22.026 cm
Vaneless diffuser width, b_5	0.582 cm
Static pressure at exit, p_5	3.88 bar
Flow angle at exit, α_5	12.55°
Tangential velocity at exit, $c_{\omega 5}$	284.36 m/s
Radial flow velocity at exit, $c_{r 5}$	63.37 m/s
Absolute flow velocity at exit, c_5	291.33 m/s
Static temperature at exit, t_5	430.28° K
Density at exit, ρ_5	3.14 kg/m ³

4. Volute Design

The last basic component of a centrifugal compressor stage is the volute or scroll. It is a spiral – shaped housing which collects the flow from the diffuser and passes it to a pipe at the exit.

Design Method

Considering the flow in the volute to be frictionless and the volute cross-section to be circular, for simplicity and ease of manufacture, the continuity equation at azimuth angle ϕ gives:

$$\dot{m}_\phi = \rho_\phi A_\phi c_{\omega\phi} \tag{52}$$

But $\dot{m}_\phi = \dot{m} \left(\frac{\phi}{360} \right)$

Since the difference in velocity at r_5 and r_ϕ is likely to be small compared to the local velocity of sound, then the density ratio will be nearly one, consequently;

$$\rho_\phi = \rho_4, c_{\omega\phi} = c_\omega \text{ and } A_\phi = \frac{\pi d_\phi^2}{4}$$

Substituting the above expressions in Eqn. 52 and re-arranging will give an expression for volute cross-section diameter at any azimuth angle as:

$$d_\phi = \left[\left(\frac{4}{\pi} \right) \left(\frac{\phi}{360} \right) \left(\frac{\dot{m}}{\rho_\phi c_{\omega\phi}} \right) \right]^{\frac{1}{2}} \tag{53}$$

For manufacturing purpose, the volute was made of two parts, the volute and its cover. Final design drawings of the volute and its cover are shown in Fig. 23 and Fig. 24 respectively.

5. Conclusion

- The design of a single stage centrifugal compressor comprising an impeller, a vaneless diffuser and the volute has been presented. The compressor has been designed as part of micro-gas turbine designed for power generation running at 60000 rpm and developing 60 kW electrical power.
- The principal geometric dimensions of the impeller and the number of blades were determined based on non-linear optimization code developed for this purpose. Also, the code was used to find the optimum axial length and optimizing the blade passage.
- The computer code for the design of the impeller was verified and the results showed quite good agreement with CFD analysis published data in the open literature.
- A procedure for designing the vaneless diffuser and the volute was given based on the governing equations of mass, momentum, and energy conservation. The flow is assumed to be isentropic and satisfies the free vortex relationship.

Notation

A	Area normal to mean flow direction (m^2)
b	Blade width (m)
B_f	Blockage factor
C	Absolute flow velocity of gas (m/s)
C_p	Specific heat capacity at constant pressure for gas (kJ/kgK)
d	Diameter (m)
f_c	Friction factor
M	Absolute Mach number
M_r	Relative Mach number
\dot{m}	Mass flow rate (kg/s)
N	Rotational speed (rpm)
N_b	Number of blades
P	Stagnation pressure (N/m^2 , bar)
R_e	Reynolds number
r_c	Radius of curvature (m)
T	Stagnation temperature (K)
t	Blade thickness (m)
u	Impeller tip velocity (m/s)
v, V	Relative velocity (m/s)
W	Work output (kJ)
z	Axial length (m)

Greek Symbols

α	Absolute flow angle relative to axial direction (degree), angle between meridional streamline and axis
β	Relative flow angle relative to axial direction

(degree), angle between relative velocity vector and meridional plane

β_b	Blade angle
θ	Relative angular co-ordinate
γ	Ratio of specific heats
η	Efficiency of a process
ρ	Gas density (kg/m^3)
Ψ	Blade loading
φ	Pressure loss coefficient
φ_s	Slip factor
ϕ	Centroid
ω	Angular velocity (rad/s)
Δ	Small increment of

Subscripts

0	Stagnation conditions
1	Impeller inlet station at mean
2	Impeller outlet station
3	Vaneless diffuser inlet station
5	Vaneless diffuser outlet station
a	Air
av	Average
c	Compressor
e	Exit condition
h	Hub
$hydr$	Hydraulic diameter
i	Inlet condition
m	Mean
SFL	Skin friction loss
DBL	Blade loading coefficient
w	Tangential direction
rms	Root mean square
r	Radial direction
x	Any station inside the rotor passage

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