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## Characterisation of Nickel Catalyst used in Urea Steam Reforming

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### Introduction

Urea is a safe and sustainable substance that is identified as being an attractive energy carrier for hydrogen [1]. Hydrogen could replace fossil fuels as an energy source by its utilisation in fuel cells [2]. Steam reforming of urea has recently been achieved and a syngas rich in hydrogen ( $H_2$ ) was produced [3]. The catalyst used in steam reforming of urea was nickel on alumina. Characterisation of this catalyst in terms of its physical nature and its efficacy at urea steam reforming is hereby reported.

### Experimental

An experimental catalytic urea steam reforming parametric study was completed in a fix bed reactor at a range of temperatures between 500°C and 700°C. A range of steam to carbon ratios (S:C) from 2:1 to 8:1 were attempted. 20 grams of 18wt% nickel oxide on alumina catalyst was used. Syngas composition was measured by a series of online analysers, and compared against thermodynamic modelling predictions calculated using EQUIL software [4]. Condensate was analysed offline for  $NH_4^+$  content. Catalyst characterisation used was determined by assessment of syngas composition over time, digital microscopy, SEM, TEM, EDX, and BET adsorption.

### Results/Discussion

$H_2$  yields close to the theoretical maximum of 3 were achieved at temperatures of 600°C. Catalyst efficiency for steam conversion and therefore  $H_2$  production reduced significantly below 600°C. At lower temperatures, the catalyst performed less well for ammonia ( $NH_3$ ) dissociation with experimental  $NH_3$  values found to be higher than equilibrium predictions.

No deactivation of the catalyst was observed with five stages of repeated steam reforming, oxidation and reduction. No catalyst deactivation was observed over the run time of the

experiments ( $\geq 2$  hours). The catalyst did not exhibit evidence of carbon deposition, increase in surface area, or the conversion of Ni to NiO during steam reforming (see Table 1 and Figure 1).

Table 1. BET results of catalyst surface area at different stages in urea steam reforming process

Condition	Surface Area
Post steam reforming	2.971 m <sup>2</sup> /g
Post steam reforming, oxidation and reduction	2.775 m <sup>2</sup> /g
Fresh oxidised (as supplied)	3.262 m <sup>2</sup> /g
Fresh reduced	3.720 m <sup>2</sup> /g

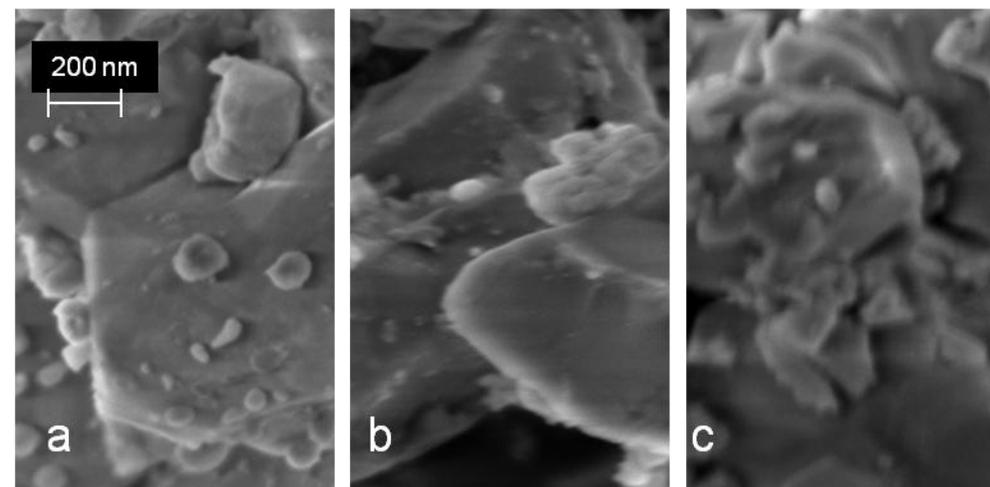


Figure 1. SEM of nickel oxide catalyst post urea steam reforming (a), reduced (b), and fresh as supplied oxidised (c).

### References.

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