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1 **Removal of metals from aqueous solutions using dried *Cladophora parriaudii***  
2 **of varying biochemical composition**

3

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## 27 **Abstract**

28 Macroalgal biosorption has shown promise for the removal of metal ions from wastewaters, whose  
29 presence can pose a threat to the aquatic environment. There is a wealth of literature published on  
30 macroalgal biosorption, the common thread being that the biosorbent material was collected from  
31 the field, under undefined conditions. These studies offer little insight into the impact of prior  
32 cultivation or biomass production practices upon the biosorbent material, its adsorptive physico-  
33 chemical properties and its subsequent capacity for metal removal. The present study sought to  
34 investigate the influence of changes in macroalgal cultivation, specifically nutrient regime, upon  
35 biomass properties and the resultant adsorption performance. The macroalga *Cladophora parriaudii*  
36 was cultivated under six different nutrient regimes; 2:1 and 12:1 N:P molar ratios, with nitrogen  
37 supplied either as ammonium ( $\text{NH}_4^+$ ), nitrate ( $\text{NO}_3^-$ ), or urea ( $\text{CO}(\text{NH}_2)_2$ ). These nutrient regimes were  
38 designed to produce biomass of varying biochemical and cell surface profiles. After cultivation, the  
39 biomass was rinsed, dried, biochemically analysed and then used for the removal of four individual  
40 metals from solution. Metal removal varied considerably between treatments and across initial  
41 metal concentrations, with removal values of 46-85%, 9-80%, 8-71%, and 49-94% achieved for Al, Cu,  
42 Mn, and Pb, respectively, with initial metal concentrations varying between 0-150 mg L<sup>-1</sup>. The  
43 observed variation in metal removal can only be attributed to differences in biochemistry and cell  
44 surface properties of the biosorbent induced by nutrient regime, as all other variables were  
45 constant. This study demonstrates that prior cultivation conditions influence the biochemistry of a  
46 biosorbent material, namely macroalgae *Cladophora parriaudii*, which has an impact upon metal  
47 removal. This aspect should be given due consideration for future biosorption research and when  
48 reviewing already published literature.

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51 **Keywords:**

52 *Cladophora*; Heavy metals; Biochemical composition; Adsorption; Copper; Macroalgae

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56 **Highlights:**

- 57 • Algal biomass composition varied with nutrient regime.
- 58 • Metal containing clusters appeared on the cell surface following metal exposure.
- 59 • Biomass of varying composition resulted in differing metal adsorption performance.
- 60 • More copper was removed from solution when biomass was rich in carbohydrates.

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73 **1. Introduction**

74 A global growing population and consequential industrial growth has led to the contamination of  
 75 numerous water bodies with toxic or heavy metals (Kotrba, 2011; Wang and Chen, 2009).  
 76 Concentrations of copper and lead in surface waters have been reported to be in excess of the  
 77 WHO's recommended drinking-water guidelines (Table 1).

78 **Table 1.** Concentrations of copper and lead found in surface waters and their permissible limits in  
 79 drinking water according to the WHO guidelines.

Water Type	Copper		Lead		References
	(mg L <sup>-1</sup> )	(mmol L <sup>-1</sup> )	(mg L <sup>-1</sup> )	(mmol L <sup>-1</sup> )	
<b>Surface Waters</b>	0.002 – 3.95	3.2 * 10 <sup>-5</sup> – 6.2 * 10 <sup>-2</sup>	0.0003 - 0.4	1.5 * 10 <sup>-6</sup> – 1.9 * 10 <sup>-3</sup>	(Kar et al., 2008; Reza and Singh, 2010; Varol and Şen, 2012)
<b>Drinking Water Quality</b>	1	3.15 * 10 <sup>-2</sup>	0.01	4.8 * 10 <sup>-5</sup>	(WHO, 2017)

80  
 81 The presence of toxic or heavy metals in water is a pertinent global problem (Ali et al., 2013; He and  
 82 Chen, 2014; Islam et al., 2015), therefore, the removal of heavy or toxic metals from wastewaters is  
 83 of paramount importance to preserve human, aquatic, and environmental health. Conventional  
 84 treatment technologies, including membrane technology, ion exchange, and activated carbon have  
 85 disadvantages, such as high capital and/or operational costs, as well as toxic sludge generation  
 86 (Fulazzaky et al., 2019, 2015; Sepehri et al., 2020). Metal ion removal efficiency can be low for  
 87 reverse osmosis (85%) and ion exchange (55%) technologies, especially when treating large volumes  
 88 of wastewater containing a low concentration of metal ions (Fu and Wang, 2011; Pap et al., 2020;  
 89 Zhang et al., 2009). This is of particular importance for wastewater polishing or wastewater tertiary  
 90 treatment since some metals are toxic even at low concentrations (Tchounwou et al., 2012).  
 91 Furthermore, ion exchange resins have to undergo chemical regeneration once they are  
 92 “exhausted”, which leads to the development of secondary waste streams (Fu and Wang, 2011).

93 Therefore, novel and sustainable processes for the removal of toxic elements from solution should  
94 be sought. An alternative for metal removal from wastewaters is biosorption (Mack et al., 2007;  
95 Utomo et al., 2016; Volesky and Holan, 1995), *i.e.* the sorption of metals using material of a  
96 biological origin, which encompasses both absorption and adsorption (Gadd, 2009). Macro-algae, in  
97 particular, are viewed as promising candidates for biosorption purposes, given their general  
98 ubiquity, abundance and high metal sorption capacity (Figueira et al., 2016; Henriques et al., 2017).  
99 Considerations into species selection, standardisation of biomass collection vs biomass production,  
100 suitability of different wastewater streams, removal of co-existing contaminants, recovery of  
101 metals/contaminants, circularity/reusability of the biosorbent material following pollutant removal,  
102 process implementation and scalability, and techno-economic and environmental life cycle  
103 assessments need to be researched.

104 There are a variety of biotic and abiotic factors which influence biosorption including pH,  
105 temperature, initial metal concentration and the presence of co-existing ions (Mehta and Gaur,  
106 2005; Özer et al., 2004). In addition, the properties of the biosorbent material will also affect metal  
107 sorption, including the species, whether it is living or not, its surface area, initial biosorbent dosage,  
108 and any pre-treatment of biomass *e.g.* immobilization or chemical modification (Camacho et al.,  
109 2013; Chojnacka et al., 2004; Figueira et al., 2016; Gadd, 2000; Özer et al., 2004; Tien, 2002).  
110 Moreover, the type and abundance of functional groups of the species studied will also have an  
111 impact upon both the type of metals/contaminants removed and overall sorption capacity (Figueira  
112 et al., 2016). It is known that differences in macro-algal culture conditions will elicit a change in the  
113 biochemical content of its biomass (Ross et al., 2018). For instance, Schiener et al., (2015) reported  
114 that across a 14 month time-frame, the tissue C and N % of wild populations of *Saccharina latissima*  
115 ranged from 21.1-30.5% and 0.8-2.2%, respectively. Therefore, differences in cultivation conditions  
116 (including nutrient regime) will influence the biochemical composition of the biomass and may result  
117 in an alteration in the quantity and quality of functional groups present on the cell surface; this in  
118 turn, may have a resultant impact upon its metal removal capacity. There is a wealth of literature

119 pertaining to metal removal with macro-algal biomass with recent results reporting removal values  
120 of 50-70%, 55-80%, and 5-97.5% for cadmium, lead, and nickel, respectively; this highlights the  
121 potential that macroalgal biomass has as a biosorbent for recalcitrant pollutants (Amro and Abhary,  
122 2019; Arumugam et al., 2020; El-Naggar and Rabei, 2020). However, minimal attention has been  
123 paid to the impact of algal cultivation conditions and/or biomass production on the resultant metal  
124 biosorption. Instead, the majority of studies focus upon the optimisation of process parameters (e.g.  
125 pH) utilising biological material of a given species that has been collected from the field (Amro and  
126 Abhary, 2019; Arumugam et al., 2020; El-Naggar and Rabei, 2020; Topal et al., 2020; Zhang et al.,  
127 2019). The drawback of these studies is that they do not provide any background information  
128 relating to the life or nutritional history of the biomass, the environmental conditions in which it was  
129 produced, age, time spent washed ashore, if it exhibits any signs of bacterial degradation or  
130 presence of epiphytes, or if it has been previously exposed to contaminants during its growth,  
131 including heavy metals. Essentially, the studies employ a biomass of unknown biochemical  
132 composition, propagated under undefined conditions for metal removal optimisation. From a  
133 wastewater treatment perspective, there is a demand for a low-cost material which can be produced  
134 in bulk and of consistent quality for contaminant removal purposes (Calderón et al., 2020; Pap et al.,  
135 2020). Previously published macroalgal biosorption studies may indicate material of a given type,  
136 collected at a given time, with potential bioremediation promise, however, they may be of negligible  
137 practical significance since there is no information provided regarding the biomass production.

138 The main aim of this study was to investigate the influence of macroalgal production practices,  
139 specifically nutrient regime, upon the quality of harvested biomass and the impact that this has upon  
140 metal removal. To test this hypothesis, *Cladophora parriaudii* was cultivated with three different  
141 nitrogen sources: ammonium ( $\text{NH}_4^+$ ) nitrate ( $\text{NO}_3^-$ ) and urea, and at two different N:P ratios (2:1 and  
142 12:1) known to produce biomass with differing bulk chemical compositions (Ross et al., 2018). The  
143 filamentous macro-alga *C. parriaudii* was selected as a model organism due to its large surface area,  
144 ubiquity, abundance, and ease of harvest making it a strong candidate species for metal removal

145 applications (Ross et al., 2017). To simplify the sorption process, the biomass produced was dried  
146 and then used for the adsorption of four different heavy or toxic metals, namely Al, Cu, Mn and Pb.  
147 These metals were selected based upon their prevalence in the environment, varying degrees of  
148 toxicity (low-high), and whether or not they have any known function within an algal cell and hence  
149 may have some uptake mechanism in place (Förstner and Wittmann, 1981; Raven et al., 1999). The  
150 experimental conditions used in this study were selected based upon optimal values obtained from  
151 an in-depth literature review (Davis et al., 2000; Lee and Chang, 2011; Prasher et al., 2004).  
152 Characterisation of biomass and metal removal analyses was conducted using a suite of biochemical  
153 and analytical methods including inductively coupled plasma optical emission spectrometry (ICP-  
154 OES), Fourier transform infrared spectroscopy (FTIR), and scanning electron microscopy with energy  
155 dispersive X-ray analysis (SEM-EDX).

156

## 157 **2. Materials and Methods**

### 158 **2.1. Algal cultivation**

159 The green filamentous macro-alga *Cladophora parriaudii* CCAP 505/09 was obtained from the  
160 Culture Collection of Algae and Protozoa (CCAP), at the Scottish Association for Marine Science  
161 (SAMS, UK). Algal biomass was incubated in an illuminated shaker (Sartorius Stedim Biotech,  
162 Germany) at 100 rpm at 24°C, under an 18:6 h L:D (Light:Dark) photoperiod, with 30-40  $\mu\text{mol}$   
163  $\text{photons m}^{-2} \text{s}^{-1}$  of photosynthetically active radiation (PAR: 400-700). Algae were grown in six  
164 variations of modified Guillard's f/2 medium (Guillard and Ryther, 1962), based on artificial seawater  
165 at 33.5 g L<sup>-1</sup> (Instant Ocean, UK) (Ross et al., 2018). Nitrogen (N) and phosphorous (P) were supplied  
166 as either ammonium (NH<sub>4</sub><sup>+</sup>), nitrate (NO<sub>3</sub><sup>-</sup>), or urea (CO(NH<sub>2</sub>)<sub>2</sub>) at 2:1 or 12:1 N:P molar ratios,  
167 corresponding to an initial N content of 160 or 960  $\mu\text{M}$ , respectively. Algal sub-cultures were pre-  
168 acclimated in experimental media and conditions for 7 days prior to the commencement of growth.



169 Triplicate 1 L flasks containing 650 mL of media were inoculated with 465 mg fresh weight *C.*  
170 *parriaudii* and maintained under the conditions described above. After 14 days, all cultures were  
171 harvested, rinsed with deionised water to remove extracellular salts and nutrients. Residual water  
172 was removed using a reticulated spinner (Ross et al., 2017). Harvested biomass was frozen and  
173 lyophilised overnight (Modulyo 4K Freeze-Dryer, Edwards, UK). This freeze-dried biomass was used  
174 as the feedstock for biosorption trials, as well as for biochemical analysis.

175

## 176 2.2. Biochemical analyses

177 Protein was extracted using hot-trichloroacetic acid and overnight incubation in an alkaline solution  
178 before quantification using the Lowry assay (Slocombe et al., 2013). Total soluble carbohydrate  
179 content of the biomass was assessed using a modified phenol-sulphuric acid method (Fournier,  
180 2001), originally described by (Dubois et al., 1956). Briefly, 2.5 mL of 1M H<sub>2</sub>SO<sub>4</sub> is added to 5 mg of  
181 dry weight (DW) biomass and acid-hydrolysed in an autoclave at 121°C for 15 min at 1.14 bar  
182 (TCR/40/H, Touchclave-R, LTE Scientific, UK). Once cooled to room temperature (RT = ~20-25°C), 30  
183 µL of the hydrolysate was reacted with 0.5 mL of 4% phenol (w/v) followed by the direct addition of  
184 2.5 mL of concentrated H<sub>2</sub>SO<sub>4</sub>. Once cooled to RT, the mixture was read in a spectrophotometer at  
185 490 nm (Helios Gamma UV-vis spectrophotometer, Thermo Scientific, UK). Pigments were extracted  
186 from biomass using a method based on (Griffiths et al., 2011), where 2 mL of dimethylsulfoxide  
187 (DMSO) was added to 1.5 mg of biomass and incubated overnight in a dark water bath at 60°C. The  
188 ash content of the biomass followed a standard method (Sluiter et al., 2008). The biochemical  
189 components were all expressed as a % DW, with any of the biomass that was unaccounted for  
190 described as “other”.

191

## 192 2.3. Stock and feed solutions

193 Heavy metal stock solutions ( $1000 \text{ mg L}^{-1}$ ) were prepared by dissolving  $\text{Al}_2(\text{SO}_4)_3 \cdot 16\text{H}_2\text{O}$ ,  $\text{CuSO}_4 \cdot 5\text{H}_2\text{O}$ ,  
194  $\text{MnCl}_2 \cdot 4\text{H}_2\text{O}$  or  $\text{PbCl}_2$  in ultrapure water ( $18.2 \text{ M}\Omega \cdot \text{cm}^{-1}$ ), with a few drops of  $\text{HNO}_3$  (Aristar<sup>®</sup> grade,  
195 VWR, UK) added to avoid metal precipitation. All powdered chemicals were obtained from Fisher  
196 Scientific (UK) and were of analytical grade (95-99%). Working metal concentrations of 1, 10, 40, 80,  
197 and  $150 \text{ mg L}^{-1}$  were created by diluting with deionised water. This concentration range was selected  
198 in order to determine the maximum sorption capacity of the biomass, rather than mimicking what is  
199 experienced in the environment. The pH was adjusted to 4.5 using either 0.1 M HCl or NaOH (Davis  
200 et al., 2000).

201

## 202 2.4. Metal sorption protocol

203 Metal sorption experiments were performed in multi-well plates housed in an incubated shaker  
204 (Sartorius Stedim Biotech, Germany) at 100 rpm,  $24^\circ\text{C}$ , and at atmospheric pressure, with a non-  
205 living biosorbent dose of  $1 \text{ g L}^{-1}$  (Lee and Chang, 2011). Experiments were incubated for 24 h to allow  
206 sufficient time for metal sorption equilibrium (Prasher et al., 2004). Algal material was then removed  
207 from the individual wells and placed in individual micro-centrifuge tubes and dried overnight in an  
208 oven at  $60^\circ\text{C}$ . The remaining metal solutions were transferred to individual centrifuge tubes and  
209 acidified with a few drops of  $\text{HNO}_3$  (Aristar<sup>®</sup> grade, VWR, UK) to prevent precipitation and  
210 subsequently analysed for metal concentration.

211

## 212 2.5. Multi-elemental analysis

213 Metal solutions were analysed by ICP-OES (Optima 5300 DV, Perkin Elmer, UK) at the School of  
214 Chemistry, University of Edinburgh (Darmovzalova et al., 2020). The ICP-OES utilised a radio  
215 frequency forward power of 1400 W, with Ar gas flows of 15, 0.2, and  $0.75 \text{ L min}^{-1}$  for plasma,  
216 auxiliary, and nebuliser, respectively. A peristaltic pump was employed to draw the sample into a

217 Gem Tip Cross-Flow Nebuliser and Scott's Spray Chamber at 1.5 mL min<sup>-1</sup>. In all instances, the  
218 instrument was operated in axial mode. On each sampling occasion, calibration standards were  
219 prepared for each metal using single element 1000 mg L<sup>-1</sup> standards (Fisher Scientific, UK), diluted  
220 with 2% HNO<sub>3</sub> (v/v) (Aristar<sup>®</sup> grade, VWR, UK). Several wavelengths were initially selected for each  
221 element and were analysed in a fully quantifiable mode (three points per unit wavelength), with  
222 three replicates employed per sample. A single wavelength for each element was selected for  
223 reporting results based upon the peak shape, background interference, sensitivity, and the linearity  
224 of the calibration curve. The selected wavelengths were 308.213 nm, 324.752 nm, 259.372 nm, and  
225 220.353 nm for Al, Cu, Mn, and Pb, respectively. All calibration curves had a linear regression of R<sup>2</sup> ≥  
226 0.99993. Blanks and internal standards were analysed periodically to ensure the accuracy of the  
227 method.

228

## 229 2.6. FT-IR analysis

230 FT-IR spectroscopy was used to detect vibrational frequency changes in algal biomass before and  
231 after metal sorption. Spectra were collected using FT-IR attenuated total reflectance (ATR) using a  
232 Perkin Elmer (UK) Frontier at the Institute for Materials and Processes, School of Engineering,  
233 University of Edinburgh. The FT-IR is equipped with a diamond crystal Universal ATR Sampling  
234 Accessory and with a mercury cadmium telluride detector. Samples were scanned over a  
235 wavenumber range of 4000 - 650 cm<sup>-1</sup> at a resolution of 2 cm<sup>-1</sup>. Approximately 1-2 mg of lyophilised  
236 biomass was placed onto the crystal surface and pressed into the crystal head at a force of 60  
237 arbitrary units. Each sample consisted of an average of 25 scans. Sample scans were recorded using  
238 Spectrum software (v. 10, Perkin Elmer), with the background automatically corrected for air and  
239 atmospheric CO<sub>2</sub>/H<sub>2</sub>O.

240

## 241 2.7. SEM analysis

242 After biosorption, dried algal biomass was mounted onto specimen stubs and coated in carbon (BTT-  
243 IV carbon evaporation coater, Denton Vacuum, USA). Samples were visualised using a scanning  
244 electron microscope (Zeiss SIGMA HD VP FE-SEM, Carl Zeiss Microscopy, UK) at the School of  
245 GeoSciences, University of Edinburgh (Manning et al., 2017). Images were recorded using the back-  
246 scattered electrons technique (BSE). SEM energy-dispersive X-ray (EDX) analysis (Aztec EDS system,  
247 Oxford Instruments) was performed on samples utilising an accelerating voltage of 20 kV, an  
248 aperture size of 30  $\mu\text{m}$ , and a working distance of  $7 \pm 1$  mm.

249

## 250 2.8. Metal removal

251 Metal sorption is primarily presented as the metal removal per unit dry weight biomass ( $\text{mmol g}^{-1}$   
252 DW) at each initial metal concentration ( $C_0$ ). The percentage of metal removal and variance in  
253 removal is also presented. To ease comparison with literature, Langmuir and Freundlich equilibrium  
254 adsorption isotherms were modelled, and the data presented in the supplementary material.  
255 The capacity of sorption by *C. parriaudii* biomass is characterised by the mass balance Equation (1):

$$256 \quad Q_e (\text{mmol g}^{-1}) = \frac{V(C_0 - C_e)}{S} \quad (1)$$

257

258 Where,  $Q_e$  is the metal sorbed at equilibrium ( $\text{mmol g}^{-1}$ ),  $V$  is the volume of solution (L),  $C_0$  and  $C_e$   
259 are the initial and final (equilibrium) concentrations in solution ( $\text{mmol L}^{-1}$ ), respectively, and  $S$  is the  
260 biosorbent dose (g). Equilibrium sorption isotherms, used to describe the relationship between the  
261 concentration of sorbed metal and metal in solution at a given temperature, were generated by  
262 plotting  $Q_e$  against  $C_e$ . The Langmuir and Freundlich models were then used to characterise  
263 biosorption. The Langmuir adsorption isotherm is described using Equation (2) (Gadd, 2009;  
264 Langmuir, 1918):

265

$$266 \quad Q_e (\text{mmol g}^{-1}) = \frac{Q_{\text{max}} \cdot b \cdot C_e}{1 + b \cdot C_e} \quad (2)$$

267

268 Where  $Q_{max}$  is the maximum adsorption capacity by the biosorbent per unit mass,  $b$  is an affinity  
269 parameter related to the energy of adsorption and indicates the strength of attraction of the sorbent  
270 for the solute (Deng et al., 2007).

271

272 The Freundlich isotherm is described using Equation (3) (Freundlich, 1907; Gadd, 2009):

$$273 \quad Q_e \text{ (mmol g}^{-1}\text{)} = K_F \cdot C_e^{\frac{1}{n}} \quad (3)$$

274

275

276 Where  $K_F$  and  $n$  are Freundlich constants and respectively relate to the adsorption capacity and  
277 adsorption intensity of the biosorbent (Deng et al., 2007). Coefficients used to describe biosorption  
278 were obtained by first linearizing equations 2 and 3.

279

## 280 2.9. Data analysis

281 All experiments were performed in triplicate, unless otherwise stated, and the experimental error  
282 was calculated and expressed as one standard deviation (SD). Data regarding the biochemical  
283 composition of the biomass is portrayed as a proportion of its dry weight (% DW). A one-way ANOVA  
284 with Tukey's post hoc analysis was used to determine significant differences in the biochemical  
285 composition of the biomass. Levels of significance were set at  $p < 0.05$ . All statistical analyses were  
286 performed using Minitab® Statistical Software version 17.

287

288

## 289 3. Results and Discussion

290 In order to understand the influence of the nutritional history on macro-algal cellular characteristics  
291 and biosorbent metal capacity, *Cladophora parriaudii* was cultivated under different nutrient  
292 regimes as described in a previous study by many of the same authors (Ross et al., 2018). After the

293 cultivation period, algal samples were harvested, dried, and biochemically characterised. Following  
294 this, four different types of metals across a concentration range, were independently adsorbed onto  
295 the dried biomass. Metals, namely Al, Cu, Mn and Pb, were selected based upon their environmental  
296 prevalence, toxicological effect, and biological role within an algal cell.

### 297 3.1. Biochemical Composition

298 The main aim of this research was to investigate the effect that the nutritional history has on algal  
299 biomass composition and how this then influences its capacity for metal removal. *C. parriaudii* was  
300 cultivated under six different nutrient regimes, designed to produce biological material of varying  
301 chemical composition: these were formulated using three different N sources ( $\text{NH}_4^+$ ,  $\text{NO}_3^-$ , and urea)  
302 supplied at two N:P ratios (2:1 and 12:1). As previously found by the authors, (Ross et al., 2018), the  
303 selected nutrient regimes, in particular the nitrogen type and N:P ratio, exerted a great influence  
304 upon the final biochemical composition of *C. parriaudii* biomass, with results shown in Table 2. For  
305 instance, biomass cultivated under a 2:1 N:P regime had a greater carbohydrate (39.6-44.2% DW)  
306 and lower protein content (8.5-10.5% DW) in comparison to that maintained under a 12:1 regime,  
307 with values ranging from 32-37.5% DW and 11.5%-13.6% DW, respectively. Biomass cultivated under  
308 a 12:1  $\text{NO}_3^-$  regime had a greater carbohydrate and lower protein yield than its molar equivalent  
309 cultivated with either  $\text{NH}_4^+$  or urea, thus making it more akin to biomass cultivated with 2:1 N:P  
310 conditions. The differences in carbohydrate and protein are statistically significant when either  $\text{NH}_4^+$   
311 or urea were employed as the N source ( $p = 0.005-0.015$ ). These nitrogen forms may be removed  
312 favourably from the growth medium due to either their lower energetic requirement for assimilation  
313 or via the provision of a supplementary carbon source (Ross et al., 2018). The uptake of these N  
314 forms would likely have been enhanced, resulting in an extended duration of N-limitation under the  
315 2:1 regime, or greater N removal from the 12:1 regime. This will have an influence on the  
316 biochemical composition. For instance, macro-algae have been found to synthesise proteins and

317 chlorophylls under N sufficiency, with a shift towards the accumulation of storage polysaccharides  
 318 when nitrogen deprived (Chopin et al., 1995).

319 Biomass grown in 12:1 N:P regimes had a marginally higher pigment content (0.9-1.1% DW) in  
 320 comparison to the 2:1 ratios (0.7-1.1% DW). The ash content of *C. parriaudii* cultivated under a 2:1  
 321 NO<sub>3</sub><sup>-</sup> regime was greater (36.7% DW) than all others which were in the range of 29.4-33.5% DW  
 322 (Table 2): however, this was not statistically significant (*n* = 1). The remaining component of the  
 323 biomass has been pooled and defined as “other” (Table 2) and will most likely comprise of  
 324 incomplete extractions or non-soluble macromolecules, lipids, uronic acids, secondary metabolites,  
 325 free amino acids, nucleic acids, and other organic material. These results indicate that the nutrient  
 326 regime has a strong influence upon the final composition of *C. parriaudii*. However, this data alone is  
 327 insufficient to ascertain if there are differences in cell surface properties and what effect this may  
 328 have on metal adsorption.

329 **Table 2.** The biochemical composition of the dry weight (DW) *Cladophora parriaudii* cultivated under  
 330 different nutrient regimes. Biochemical components that are denoted by different letters are  
 331 statistically significant (*p* < 0.05).

Biochemical Component (% DW)	NH <sub>4</sub> <sup>+</sup>		NO <sub>3</sub> <sup>-</sup>		Urea	
	2:1	12:1	2:1	12:1	2:1	12:1
Ash	33.5	29.4	36.7	31.4	31.8	32.0
Carbohydrate	44.2 <sup>a</sup>	34.0 <sup>bc</sup>	39.6 <sup>abc</sup>	37.5 <sup>abc</sup>	41.0 <sup>ab</sup>	32.0 <sup>c</sup>
Pigments	0.8 <sup>a</sup>	1.1 <sup>a</sup>	1.1 <sup>a</sup>	0.9 <sup>a</sup>	0.7 <sup>a</sup>	1.0 <sup>a</sup>
Protein	8.5 <sup>b</sup>	13.3 <sup>a</sup>	10.5 <sup>ab</sup>	11.5 <sup>ab</sup>	9.5 <sup>ab</sup>	13.6 <sup>a</sup>
Other	13.1 <sup>bc</sup>	22.1 <sup>a</sup>	12.3 <sup>c</sup>	18.6 <sup>abc</sup>	17.0 <sup>abc</sup>	21.3 <sup>ab</sup>

332

### 333 3.2. Metal Removal

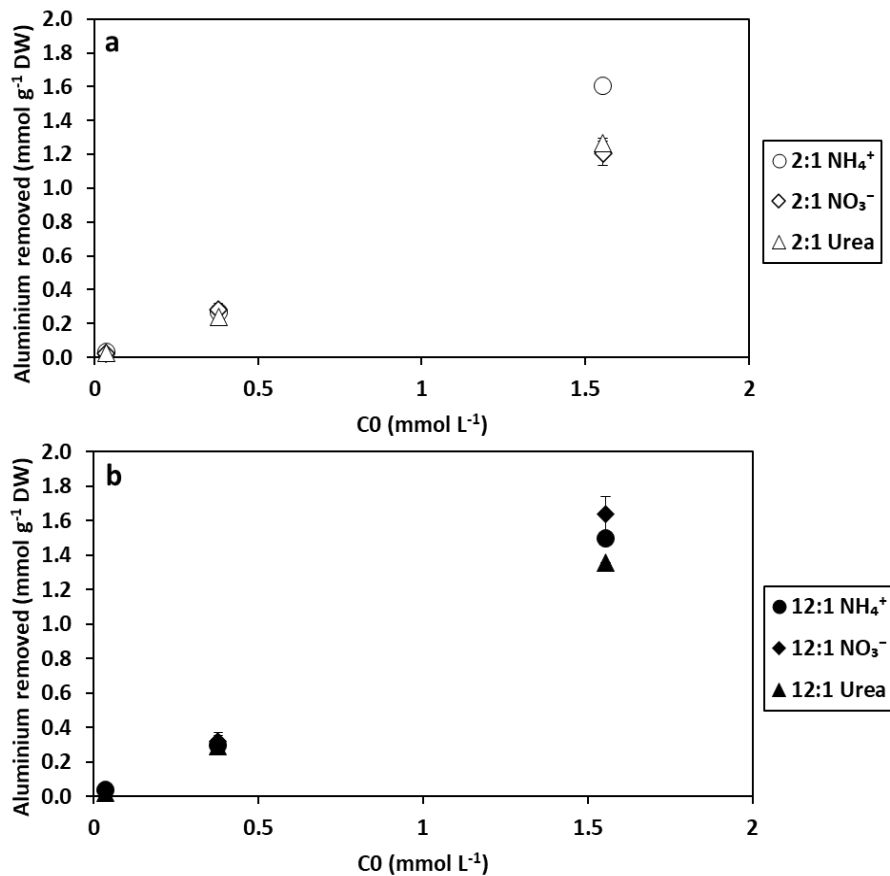
334 Experiments were performed in order to determine whether there was a difference in metal  
 335 removal performance by non-living *C. parriaudii* biomass after cultivation under six different nutrient  
 336 regimes. To test the removal capacity of Al, Cu, Mn, and Pb, were independently tested across a

337 range of working concentrations (1-150 mg L<sup>-1</sup>). In this study, sorption is principally presented as the  
338 concentration of metal sorbed per unit of dried biomass (mmol g<sup>-1</sup>) and as a proportion of metals  
339 removed from solution (Figs 1-4), as described in section 2.8. For the purpose of comparison with  
340 literature, Langmuir and Freundlich adsorption isotherms were modelled as well, with isotherm  
341 parameters shown in (Supplementary Information Table S1). These models have their deficiencies  
342 when used to describe adsorption using a biological material. For instance, the Langmuir model  
343 assumes that sorption occurs as a monolayer, while Freundlich assumes a constant pH which is very  
344 unlikely in an unbuffered system where ion exchange will result in H<sup>+</sup> displacement by binding  
345 cations (Gadd, 2009; Mehta and Gaur, 2005).

346 There was a broad variation in the biosorption capacity between both metals and nutrient regimes.  
347 Metal removal per unit biomass ranged from 0.023-1.636 (Q<sub>max</sub> = 1.08-2.35), 0.005-0.885 (Q<sub>max</sub> = 0.3-  
348 0.62), 0.005-0.658 (Q<sub>max</sub> = 0.22-0.48), and 0.002-0.855 (Q<sub>max</sub> = 0.43-0.61) mmol g<sup>-1</sup> DW for Al, Cu, Mn,  
349 and Pb, respectively (Figs 1-4 & Supplementary Table S1). These equate to 45.7-82.5%, 9.2-79.9%,  
350 8.2-71.3%, and 48.8-93.7% removal of the initial metal concentration (C<sub>0</sub>), respectively. These  
351 results are comparable to maximum removal values (Q<sub>max</sub>) for single metal solutions recorded  
352 elsewhere with other macroalgal biosorbents: of 2.79-2.865 (Lee et al., 2004; Sari and Tuzen, 2009) ,  
353 0.266-1.61 (Deng et al., 2006; Romera et al., 2007) , 0.7–1.07 (Henriques et al., 2011;  
354 Vijayaraghavan and Joshi, 2014), and 0.139-1.815 (Holan and Volesky, 1994; Pavasant et al., 2006)  
355 mmol g<sup>-1</sup> DW for Al, Cu, Mn, and Pb, respectively. While the values obtained within this study are  
356 generally within range of those reported elsewhere, direct comparison with these studies may be  
357 unfair. Most of these studies focussed upon the optimisation of process parameters (e.g. pH,  
358 temperature) with their given material to maximise metal removal, while this approach was not  
359 undertaken within this study. As a result, the metal removal values presented in this study may be  
360 an underestimation of the theoretical maximum. Furthermore, a common feature of all the above  
361 cited literature is that they all employ biomass collected from the field and do not provide any



362 background information relating to its propagation. Whilst some of the recorded values are high and  
 363 show promise for metal removal purposes, the removal values were obtained with a biomass  
 364 collected at a very particular time under undefined environmental conditions. Therefore, producing  
 365 a biomass with the same qualities for scientific reproducibility or practical application, such as  
 366 wastewater treatment, would be challenging. The importance of knowledge underpinning biomass  
 367 production is demonstrated within this study, as variation in metal sorption between treatments can  
 368 only be attributed to differences in the biochemical and structural composition of the *Cladophora*  
 369 biomass, elicited by variability in nutrient regime provided, since all other experimental process  
 370 factors were constant.



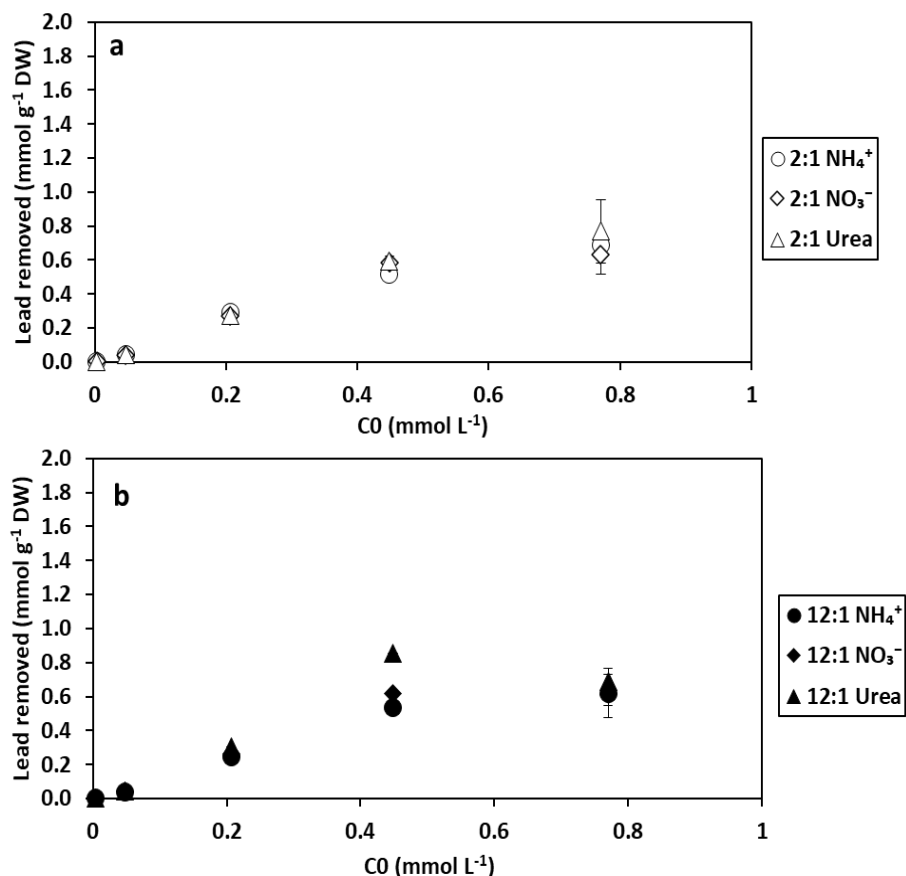
371

372 **Figure 1.** Aluminium removal per unit dry weight (DW) by *Cladophora parriaudii* biomass previously  
 373 cultivated under different N:P ratios and nitrogen types; (a) 2:1 NH<sub>4</sub><sup>+</sup> (white circle), 2:1 NO<sub>3</sub><sup>-</sup> (white  
 374 diamond), 2:1 urea (white triangle), (b) 12:1 NH<sub>4</sub><sup>+</sup> (black circle) 12:1 NO<sub>3</sub><sup>-</sup> (black diamond), 12:1 urea  
 375 (black triangle). The sorption conditions were; pH = 4.5, contact time = 24 h, biosorbent dose = 1 g L<sup>-1</sup>

376 <sup>1</sup>, agitation = 100 rpm, initial metal concentration (C<sub>0</sub>) = 0.035-1.55 mmol L<sup>-1</sup>, temperature = 24°C,  
377 light = constant with 30-40 μmol photons m<sup>-2</sup> s<sup>-1</sup> (n = 1-3, error bars = 1 SD).

378

379 Removal of aluminium and lead followed an almost linear trend, albeit with a slight plateau  
380 occurring with lead, with similarity in metal removal at all initial metal concentrations, and  
381 irrespective of the nutrient regime in which the biomass was previously cultivated under (Figs. 1 &  
382 2). This was coupled with very low levels of variance for both Al (<0.0304) and Pb (<0.0096). Neither  
383 aluminium nor lead serve any known function within the algal cell, therefore, it could be postulated  
384 that metal bonding may be indiscriminate with no preference exhibited for certain types of  
385 functional groups or specific uptake channels. Results reported elsewhere verify this, by  
386 demonstrating that a multitude of different functional groups are involved in the adsorption of  
387 aluminium and lead, including amide, carbonyl, carboxyl, hydroxyl, and sulfonate (Amro and Abhary,  
388 2019; Sari and Tuzen, 2009). This suggests that the biological influence may play a lesser role with  
389 non-essential metals.



390

391 **Figure 2.** Lead removal per unit dry weight (DW) by *Cladophora parriaudii* biomass previously  
 392 cultivated under different N:P ratios and nitrogen types; (a) 2:1 NH<sub>4</sub><sup>+</sup> (white circle), 2:1 NO<sub>3</sub><sup>-</sup> (white  
 393 diamond), 2:1 urea (white triangle), (b) 12:1 NH<sub>4</sub><sup>+</sup> (black circle) 12:1 NO<sub>3</sub><sup>-</sup> (black diamond), 12:1 urea  
 394 (black triangle). The sorption conditions were; pH = 4.5, contact time = 24 h, biosorbent dose = 1 g L<sup>-1</sup>,  
 395 agitation = 100 rpm, initial metal concentration (C0) = 0.004-0.78 mmol L<sup>-1</sup>, temperature = 24°C,  
 396 light = constant with 30-40 μmol photons m<sup>-2</sup> s<sup>-1</sup> (n = 1-3, error bars = 1 SD).

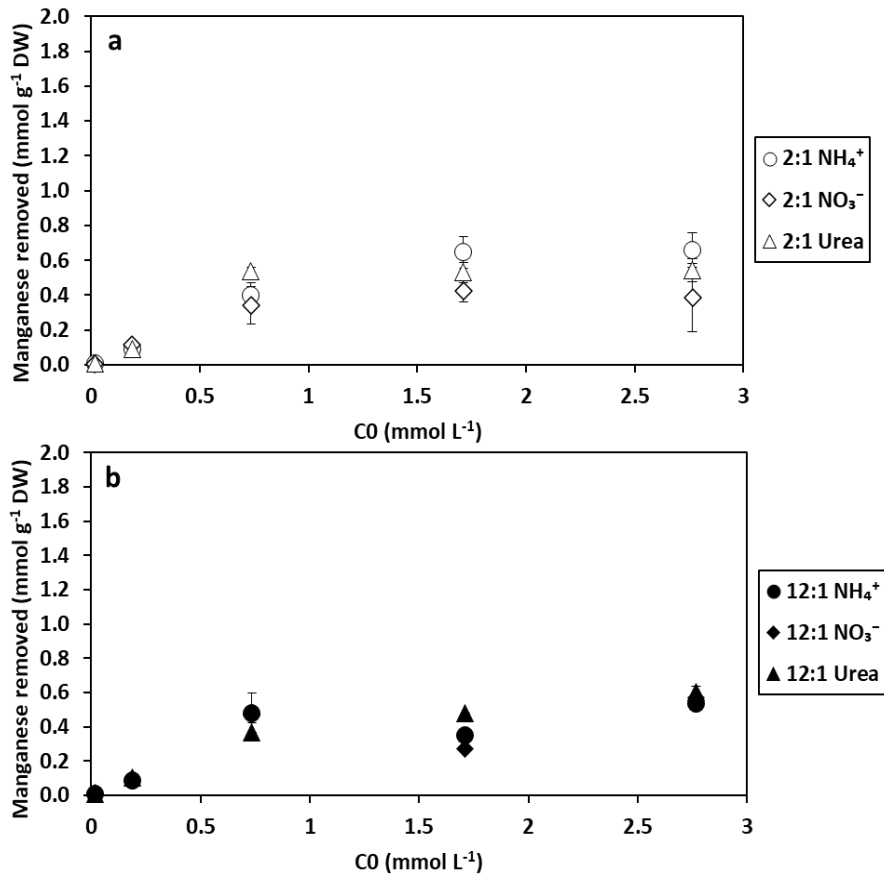
397

398 On the other hand, copper and manganese removal followed a linear trend until reaching a more  
 399 pronounced plateau (Figs 3 & 4), suggesting that the biosorbent material reached its metal  
 400 adsorption saturation capacity upon exposure to 40-80 mg L<sup>-1</sup>. This is somewhat earlier than what  
 401 was observed with aluminium and lead (Figs 1 & 2). There are several putative reasons for this.  
 402 Firstly, Cu and Mn are trace metals that are essential for algal growth, being involved in electron  
 403 transport and oxygen evolution during photosynthesis (Blaby-Haas and Merchant, 2012; Sauer,  
 404 1980). These metals may preferentially bind to specific sites on the cell surface, for instance channel

405 transporters or phytochelatins (Navarrete et al., 2019). Secondly, the *C. parriaudii* biomass was  
406 previously cultivated in f/2 medium which contains trace concentrations of Cu and Mn (Guillard and  
407 Ryther, 1962). Therefore, despite rinsing with deionised water after cultivation, the biomass would  
408 have contained these metals both intra- and extra-cellularly. This will likely have resulted in an  
409 underestimation of the capacity for the biomass to remove these metals. In comparison to Al and  
410 Pb, there was greater variability in metal removal both between nitrogen type and N:P ratio for  
411 these essential metals. However, low variability was observed in Mn removal when the biosorbent  
412 had been cultivated under a 12:1 N:P ratio (Fig. 3b), which translated to a more protein-rich biomass  
413 (Table 2). The inverse is true of copper (Fig. 4), where the greatest removal coupled with low  
414 variability in metal removal occurred when the biomass had been previously cultivated under a 2:1  
415 N:P regime or with 12:1  $\text{NO}_3^-$ . These biomass types have greater yields of carbohydrates (37.5-44.2%  
416 DW) compared to those cultivated with 12:1 N:P with  $\text{NH}_4^+$  or urea as the N source (<34% DW)  
417 (Table 2). This suggests that copper may be more strongly attracted to functional groups associated  
418 with cell wall and membrane mono- and poly-saccharides. Functional groups associated with these  
419 structural carbohydrates (e.g. hydroxyl and carboxyl) have been reported to be involved in metal  
420 removal by the green macro-alga *Codium vermilara* (Fawzy, 2020).

421 These results illustrate the influence that biochemistry and methods for producing biomaterial used  
422 in biosorption research has and may explain the broad variation in results reported in literature,  
423 especially since there is a paucity of information relating the production of the material used in this  
424 scientific discipline. However, to more fully understand this, more analyses of the cellular properties  
425 is required.

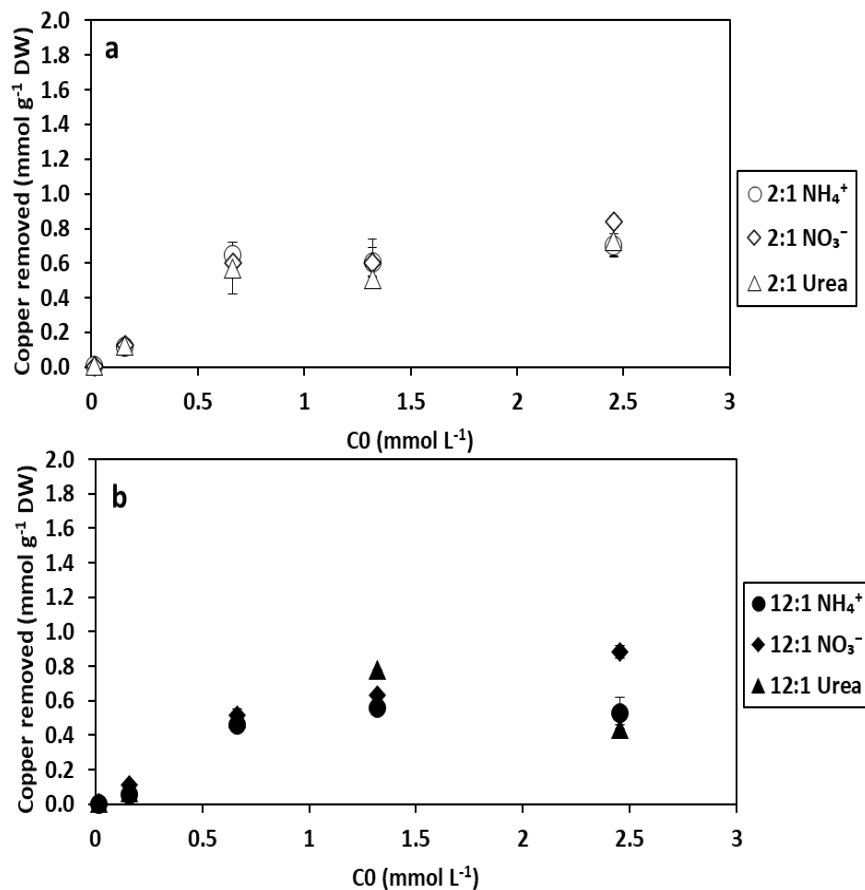
426



427

428 **Figure 3.** Manganese removal per unit dry weight (DW) by *Cladophora parriaudii* biomass previously  
 429 cultivated under different N:P ratios and nitrogen types; (a) 2:1 NH<sub>4</sub><sup>+</sup> (white circle), 2:1 NO<sub>3</sub><sup>-</sup> (white  
 430 diamond), 2:1 urea (white triangle), (b) 12:1 NH<sub>4</sub><sup>+</sup> (black circle) 12:1 NO<sub>3</sub><sup>-</sup> (black diamond), 12:1 urea  
 431 (black triangle). The sorption conditions were; pH = 4.5, contact time = 24 h, biosorbent dose = 1 g L<sup>-1</sup>,  
 432 agitation = 100 rpm, initial metal concentration (C0) = 0.016-2.77 mmol L<sup>-1</sup>, temperature = 24°C,  
 433 light = constant with 30-40 μmol photons m<sup>-2</sup> s<sup>-1</sup> (n = 1-3, error bars = 1 SD).

434



435

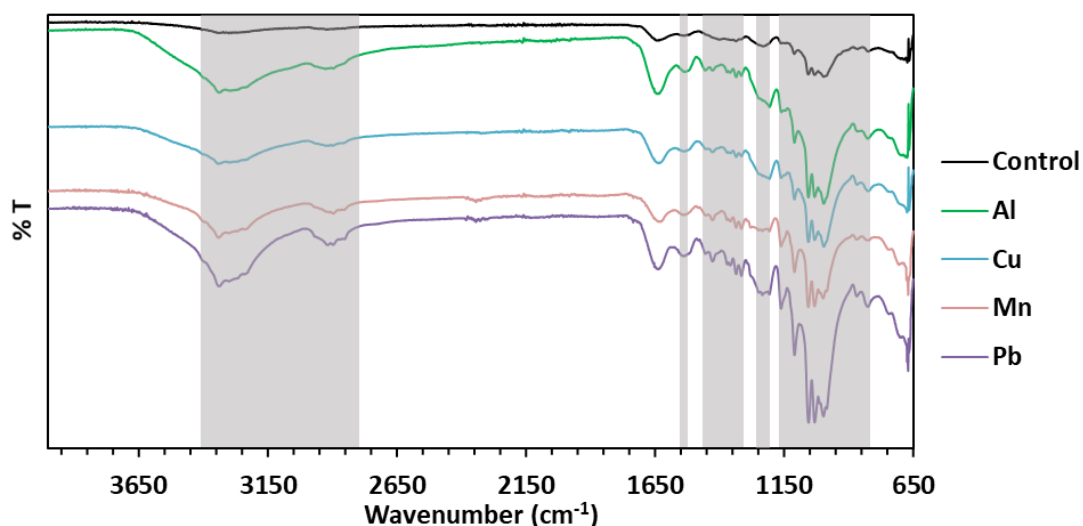
436 **Figure 4.** Copper removal per unit dry weight (DW) by *Cladophora parriaudii* biomass previously  
 437 cultivated under different N:P ratios and nitrogen types; (a) 2:1 NH<sub>4</sub><sup>+</sup> (white circle), 2:1 NO<sub>3</sub><sup>-</sup> (white  
 438 diamond), 2:1 urea (white triangle), (b) 12:1 NH<sub>4</sub><sup>+</sup> (black circle) 12:1 NO<sub>3</sub><sup>-</sup> (black diamond), 12:1 urea  
 439 (black triangle). The sorption conditions were; pH = 4.5, contact time = 24 h, biosorbent dose = 1 g L<sup>-1</sup>,  
 440 agitation = 100 rpm, initial metal concentration (C<sub>0</sub>) = 0.015-2.45 mmol L<sup>-1</sup>, temperature = 24°C,  
 441 light = constant with 30-40 μmol photons m<sup>-2</sup> s<sup>-1</sup> (n = 1-3, error bars = 1 SD).

442

### 443 3.3. FT-IR Spectra of *C. parriaudii*

444 The absorbance spectra of the *C. parriaudii* biomass pre- and post- metal exposure was obtained for  
 445 all nutrient regimes. However, since the spectra appeared very similar between treatments, only  
 446 data relating to a 2:1 NO<sub>3</sub><sup>-</sup> regime is presented here as an exemplar (Fig. 5). The FT-IR spectra for all  
 447 other regimes can be found in the Supporting Information.

448 The spectra from biomass without exposure to metals had a similar distribution of peaks, peak  
449 shape, and wavenumber, regardless of cultivation regime. The spectra presented here (Fig. 5) are  
450 very similar to those obtained from *Cladophora glomerata* biomass (Michalak et al., 2018) or from a  
451 variety of cellulosic powders from *C. glomerata* (Suciyati et al., 2021). There were strong bands  
452 present in the range of 3400-2800  $\text{cm}^{-1}$ , which can be attributed to functional groups present in  
453 proteins, lipids, carbohydrates and cellulose. There were intense peaks at 1650-1630  $\text{cm}^{-1}$  and 1550-  
454 1530  $\text{cm}^{-1}$  caused by amine groups I and II, respectively. There were a variety of peaks in the range of  
455 1460-1310  $\text{cm}^{-1}$  that can be assigned to functional groups arising from cellulose, proteins, lipids, and  
456 sulphur-containing components. There was a prominent peak at 1250-1210  $\text{cm}^{-1}$  attributed to amine  
457 group III and phosphodiester bonding of phospholipids. The remaining peaks at this lower end of the  
458 spectrum can mostly be assigned to mono- and poly-saccharides, cellulose, aliphatics of the cell wall  
459 and aromatic compounds (Fig. 5). Coupling the differences in biochemical composition (Table 2) and  
460 the comparability of FTIR-ATR spectra between treatments (Fig. 5 & Supplementary Information)  
461 suggests that cultivation under different nutrient regimes yields biomass of varying composition;  
462 however, this does not necessarily translate into the synthesis of different molecules between  
463 different nutrient regimes, but more likely in the quantity or proportion of molecules or functional  
464 groups being different. This has been demonstrated in studies that have measured the IR spectra of  
465 micro-organisms temporally and, therefore, of varying biochemical composition (Ami et al., 2014;  
466 Dean et al., 2010). Unfortunately, this cannot be verified within this study using the employed FTIR-  
467 ATR method since the algal biomass sample preparations were non-homogenous and, as such, they  
468 did not meet the implicit requirements for Beer's Law (Griffiths, 2006): the FTIR-ATR analysis should  
469 hence be considered as qualitative only, rather than quantitative. Therefore, comparison between  
470 spectra is limited to the presence/absence of bands, shifts in wavenumber, or the relative peak size  
471 within an individual spectrum.



472

473 **Figure 5.** The Infrared spectra of *C. parriaudii* biomass after cultivation under a 2:1  $\text{NO}_3^-$  regime  
 474 obtained before (black) and after metal adsorption with aluminium (green), copper (blue),  
 475 manganese (pink), and lead (purple). Each line is an average of 25 scans, baseline corrected and  
 476 atmospheric  $\text{CO}_2/\text{H}_2\text{O}$  removed. To prevent overlap between spectra and to ease visualisation, a  
 477 constant correction factor has been applied to the % transmission (% T). The main wavenumber  
 478 ranges involved in metal adsorption across treatments have been highlighted in grey.  
 479

480 After metal sorption, the IR spectra were obtained from the metal loaded biomass (Fig. 5 and  
 481 Supporting Info). Although the spectra from metal loaded biomass appeared near identical to those  
 482 without any metal exposure, there are some subtle, yet consistent, differences between them. This  
 483 indicates that certain functional groups were always involved in metal sorption. For instance, after  
 484 exposure to all metals tested, the intense peak at amine III and phosphodiester peak  $1250\text{-}1210\text{ cm}^{-1}$   
 485 changed shape, suggesting that the phospholipid membrane is involved in metal sorption. The amine  
 486 peak at  $1409\text{-}1403\text{ cm}^{-1}$ , visible in metal-free biomass, was not present in all metal loaded biomass:  
 487 instead, there was the emergence of six smaller peaks within the same region. In addition, an  
 488 increase in relative intensity was observed between  $3347\text{-}3334\text{ cm}^{-1}$ , which can be attributed to  
 489 symmetric stretching of N-H and O-H bonds within amide group A, water, and polysaccharides  
 490 including cellulose (Duygu et al., 2012; Suciayati et al., 2021). There were frequent, yet inconsistent,  
 491 changes in peak shape or wavenumber in the regions of  $3405\text{-}3390\text{ cm}^{-1}$  which is assigned to  
 492 stretching of -OH groups of water;  $2920\text{-}2850\text{ cm}^{-1}$  caused by stretching of CH,  $\text{CH}_2$  and  $\text{CH}_3$  groups



493 present in fatty acids and polysaccharides; 1650-1630  $\text{cm}^{-1}$  assigned to functional groups relating to  
494 amide group I and the relative intensity of the peaks at 1160  $\text{cm}^{-1}$  and 1056-990  $\text{cm}^{-1}$ , which were  
495 assigned to cellulose and polysaccharides, respectively. Since these changes in the FTIR-ATR spectra  
496 are inconsistent between treatments, they are likely to be indicative of the differences in  
497 relationships between the metal removal and biochemical data discussed earlier. Similar results  
498 were recorded by (Michalak et al., 2018) with *Cladophora*, where carboxyl and hydroxy groups in the  
499 regions of 1500-1400 and 1280-1200  $\text{cm}^{-1}$  were effective for the removal of Mg, Mn, and Cr ions.

500 Following copper biosorption, there was a strong reduction in relative peak intensities with  
501 functional groups associated with carbohydrates (*e.g.* 1056 and 1033  $\text{cm}^{-1}$ ) when the biomass was  
502 cultivated under a 2:1 N:P regime or with a 12:1  $\text{NO}_3^-$  as the nitrogen source. These nutrient regimes  
503 yielded biomass with elevated carbohydrate content (37.5-44.2% DW versus 32-34% DW) (Table 2)  
504 and was coincident with greater metal removal (0.704-0.885  $\text{mmol g}^{-1}$  DW versus 0.435-0.53  $\text{mmol g}^{-1}$   
505 DW) (Fig. 3). This suggests that copper has a stronger affinity for functional groups present in  
506 polysaccharides and that carbohydrate rich biomass is suitable for its removal.

507

508 Similarly, the biomass with the greatest Mn removal was propagated under either 2:1  $\text{NH}_4^+$  or 12:1  
509 urea regime (Fig. 4). This biomass was characterised by having either a high proportion of  
510 carbohydrates or protein, and consequently there was evident reduction in peak intensities at 1637,  
511 1056, 1033, and 998  $\text{cm}^{-1}$  that are assigned to functional groups associated with these  
512 macromolecules. All of these functional groups that are involved in metal biosorption are assigned  
513 to carbohydrates, proteins, and other macromolecules that may be located in or around the cell wall  
514 and membrane. A similar result has been found in the literature where there was a significant  
515 increase in removal capacity of chitinous material when associated proteins were also present with  
516 amine and carboxylic functional groups principally involved in sorption (Robinson-Lora and Brennan,  
517 2010).

### 518 3.4. SEM Analysis

519 In order to understand if metal biosorption was influenced by the surface of the cell, or if metal  
520 bonding was localised to specific sites, SEM-BSE micrographs were taken of the *C. parriaudii* biomass  
521 after metal exposure (Fig. 6). Since all micrographs appeared similar visually, the micrograph  
522 depicting biomass cultivated with a 2:1 NO<sub>3</sub><sup>-</sup> regime is used as an exemplar, with all other  
523 micrographs available in the Supporting Information. There was no apparent difference in the  
524 cellular structure between nutritional treatments with all filaments being nonporous, yet appearing  
525 furrowed or grooved, which was assumed to be due to the lyophilisation procedure prior to metal  
526 exposure. This indicates that neither the nutrient regime, nor metal type influenced the gross  
527 cellular morphology or surface topography of the cell. In addition, the SEM-BSE micrographs  
528 revealed that there were bright *clusters* present on the cell surface (Fig. 6), with EDX analysis  
529 indicating that heavy metals were present within these clusters (Fig. 7). Furthermore, these clusters  
530 were of irregular size and shape and occurred randomly across the filament surface and not confined  
531 to specific locations (*e.g.* furrows or damaged areas). These micrographs suggest that nutrient  
532 regime has little to no impact upon cell surface topography, which in turn has a minimal influence on  
533 metal biosorption.

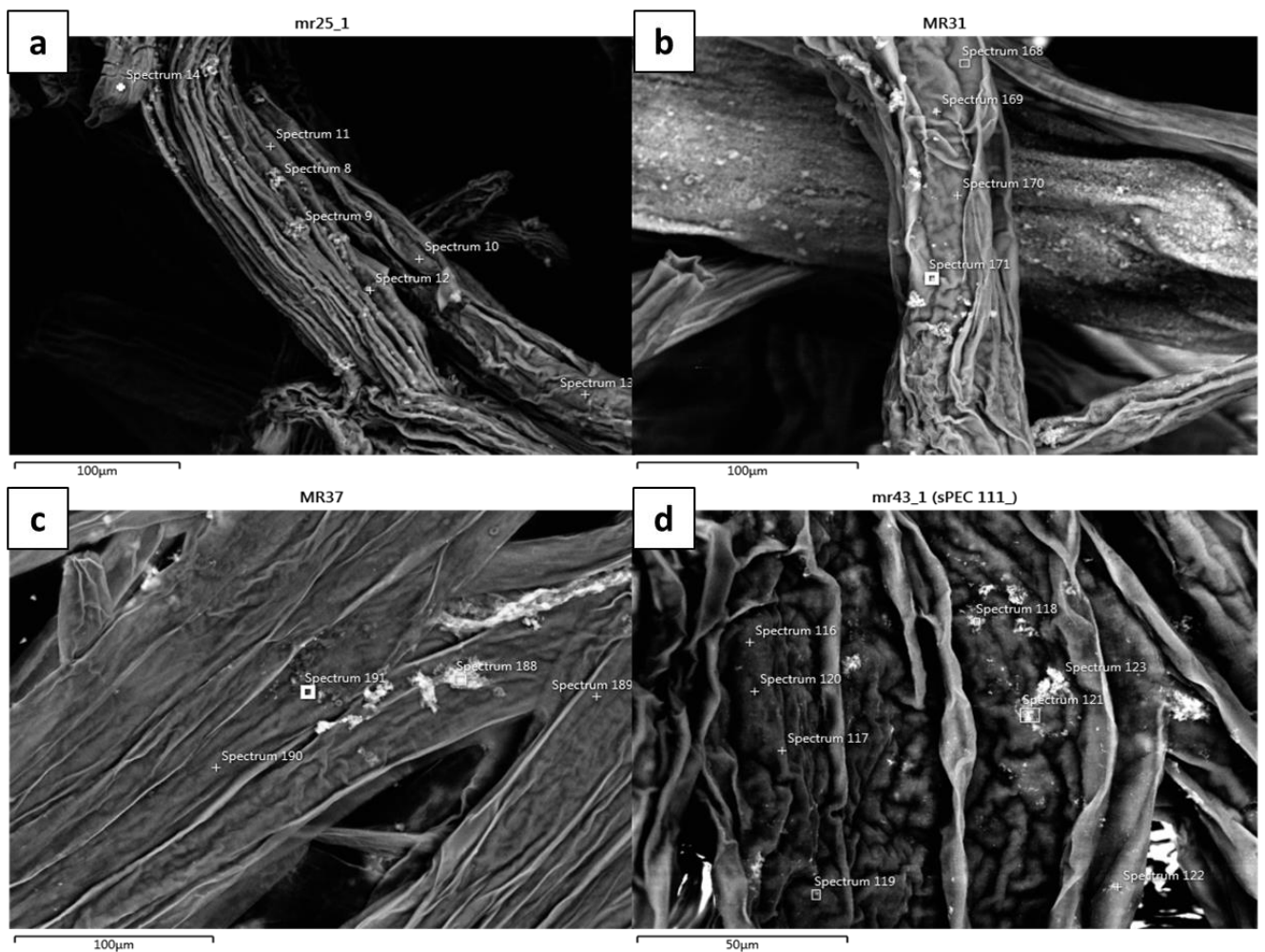
534 The elemental spectra of different surface locations of each sample was determined by EDX (Fig. 7).  
535 Specifically, in order to avoid any potential inter-sample variation in biochemical composition,  
536 spectra were obtained from areas of the cell surface where metals were thought to be less prevalent  
537 (*i.e.*, without clear visual evidence of clusters) (Fig. 7a, c, e, and g). All samples from these cell  
538 localities contained elements expected within algal biomass, including a high proportion of oxygen  
539 and sulphur, as well as phosphorus. Light and alkaline metals such as sodium, magnesium, and  
540 calcium were also present, which are elements required for the normal functioning of the algal cell.  
541 Similar elements were also found in native *Cladophora* biomass analysed by EDX analysis (Amro and  
542 Abhary, 2019). Unfortunately, the study by (Amro and Abhary, 2019) did not reanalyse the EDX

543 spectra after the biomass was used for the sorption of lead and cadmium ions, meaning that  
544 potential mechanisms of metal removal may have been overlooked. In this study, the target heavy  
545 metals were detected upon all areas of the biomass following sorption, albeit to a relatively low  
546 degree, which suggests that the whole surface of the biomass was involved in metal sorption.  
547 However, EDX spectra was measured at locations of the cell where the clusters were present (Fig.  
548 7b, d, f, and h). Signals for the target heavy metals used in this study were generally greater in these  
549 areas, hence indicating that these metals were predominantly present within these clusters. In the  
550 vast majority of instances, the spectra from the clusters (Fig. 7b, d, f, and h) contained stronger  
551 signals for O, P, Fe compared to other areas of the cell. The clusters also frequently contained  
552 stronger signals of Mg, Ca, and Si, suggesting a variety of mechanisms for metal sorption including  
553 ion exchange, complexation and micro-precipitation (Gadd, 2009; Mehta and Gaur, 2005). These  
554 elements all serve key functions within the cell. For instance, Mg is the core ion in chlorophylls  
555 located in membrane-bound chloroplasts in close proximity to the cell surface (Brock, 1973). Iron  
556 has numerous functions within the cell, including nitrogen assimilation via ferredoxin (Raven et al.,  
557 1999), whereas, P is a key constituent of the phospholipid bilayer of cell membranes (Ami et al.,  
558 2014), which FTIR analysis (Fig. 5) indicated that the component phosphodiester bonds, at 1250-  
559 1210  $\text{cm}^{-1}$ , play a role in biosorption. Studies have improved the ion exchange capacity of biosorbent  
560 material by pre-treating it with calcium (Davis et al., 2003), explaining why metals have a preference  
561 for areas with strong Ca. Silicon, on the other hand, is thought to have a healing or protective role in  
562 sporophytes of *Saccharina japonica* (Mizuta and Yasui, 2012). Si also has stress alleviation roles in  
563 higher plants by complexing, co-precipitating, or compartmentalising (toxic) metals or via  
564 stimulation of antioxidant systems (Liang et al., 2007). It was also noted that there was often a  
565 reduction in the relative proportion of S within the clusters. This was especially true after exposure  
566 to copper. The cell wall of *Cladophora* contains sulphated polysaccharides (Arata et al., 2017), and  
567 given that carbohydrate rich biomass was the most effective for the removal of copper (Table 2 &  
568 Fig. 3), it is likely that cell wall associated sulphated polysaccharides were involved in copper

569 sorption. These elements with varying signal after sorption, identified by EDX analysis, are pivotal for  
570 photosynthesis, protein synthesis, and cellular structure. All occur in or around the cell surface and  
571 are influenced by age, nutrient regime, cultivation conditions, and seasonality (Kumar and Sahoo,  
572 2017; Schiener et al., 2015), which could have significant implications when utilising material  
573 collected from the field. For instance, (Kumar and Sahoo, 2017) showed age and seasonal related  
574 variability in the Ca, Mg, and Fe (among others) content of *Sargassum wightii* biomass.

575

576

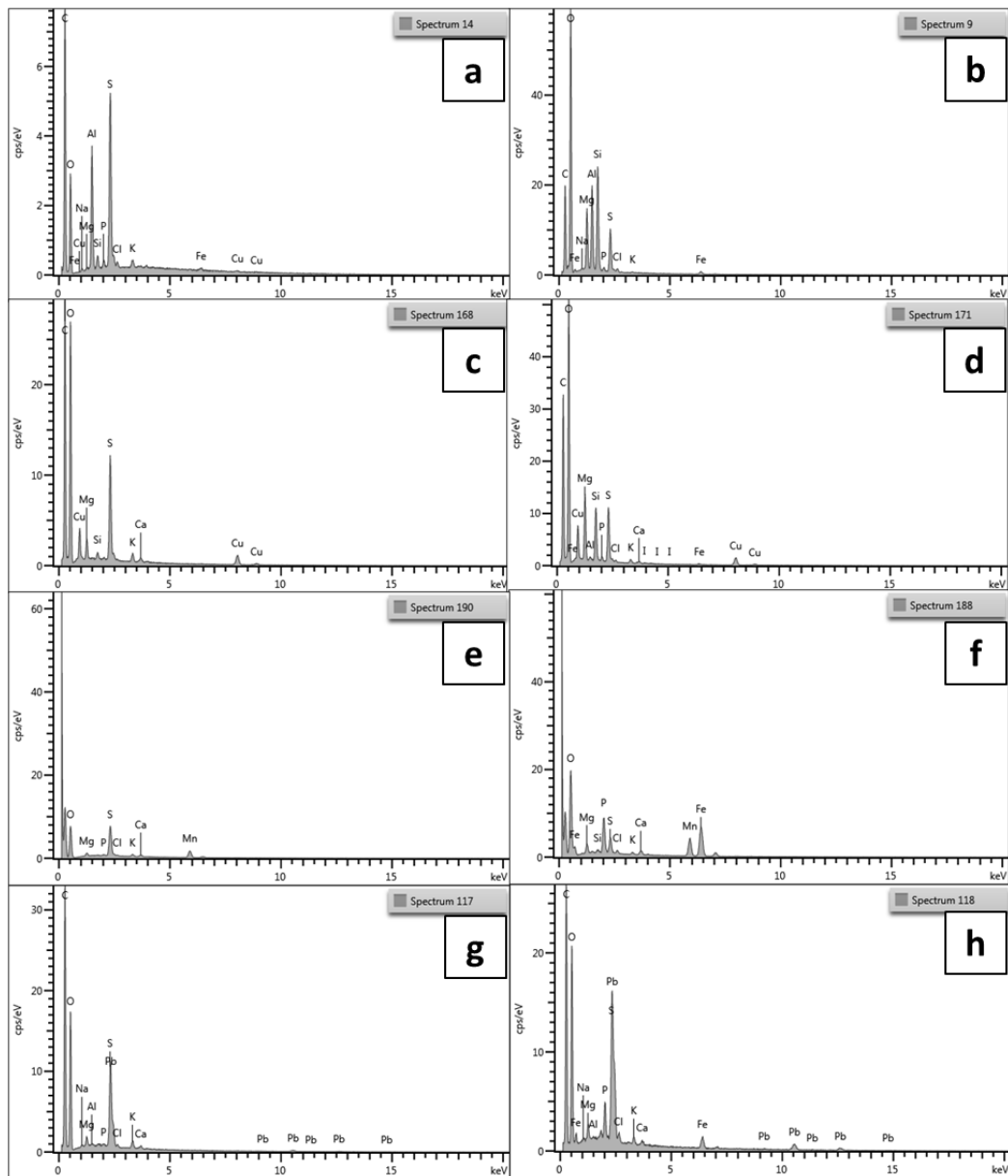


577

578 **Figure 6.** The cell surface of *Cladophora parriaudii*, previously cultivated under a 2:1 NO<sub>3</sub><sup>-</sup> medium,  
579 after exposure to a) Al, b) Cu, c) Mn, d) Pb. Images were attained with Scanning Electron Microscopy  
580 using the back-scattered electrons (BSE) technique at 20 kV and ~1.2-1.5 K x magnification. This

581 figure depicts the similarity in surface structure, regardless of the nutrient regime. Note the  
582 presence of bright irregularly shaped *clusters* scattered randomly across the surfaces of all of the  
583 filaments.

584



585

586 **Figure 7.** The Scanning Electron Microscopy – Energy Dispersive X-Ray elemental spectra of  
587 *Cladophora parriaudii*, previously cultivated under a 2:1 NO<sub>3</sub><sup>-</sup> nutrient regime and after exposure to  
588 metals: Al (a & b), Cu (c & d), Mn (e & f), Pb (g & h). The spectra on the left-hand side (a, c, e, and g)  
589 were obtained from areas on the cell surface which were deemed “pristine”, or as having no visual  
590 evidence of metal/contaminant bonding. Spectra on the right-hand side (b, d, f, and h) were  
591 obtained from areas on the cell surface in which metal was present, typically as a bright “cluster”.  
592 The specific locations of each spectrum are denoted in the corresponding images in Fig. 1. Please  
593 note differences in the y-axes.

594 By taking a holistic overview of this research and combining the clustering behaviour of metals from  
595 the SEM-BSE micrographs (Fig. 6), their FTIR-ATR and EDX spectra (Fig. 7), the biochemical  
596 composition of the biomass (Table 2), the roles of each element within the cell and a review of the  
597 literature, there are multiple mechanisms involved in adsorption, which is a very complex process.  
598 However, this complexity offers a variety of avenues of further research which lead on from this  
599 study. These include the development of a quantifiable method for the FTIR analysis, as correlating  
600 this empirically with biochemical and metal sorption values would be beneficial (Mayers et al.,  
601 2014). Investigating the impact of different nutrient regimes upon the optimised metal removal  
602 parameters (e.g. pH, temperature), in addition to the influence of counter ions within the metallic  
603 salts provided (e.g. chloride or sulphate)(Michalak et al., 2018), would also be important to assess  
604 the maximum adsorption capacity of the biomass. It would also be interesting to investigate the  
605 effects of C:N ratio during cultivation to determine if this has any resultant and beneficial impact  
606 upon biomass production in terms of yield and of extracellular polymeric substances (EPS), which  
607 would play a role in metal sorption (Gupta and Diwan, 2017; Sepehri et al., 2020). Similarly, the  
608 impacts upon different nutrient regimes upon living material biomass production, used for  
609 simultaneous metal removal, to assess if these can enhance toxicity or lead to detoxification and  
610 enhanced viability and biomass production. Greater understanding of the mechanisms involved with  
611 sorption and better description of the biosorbent material by adopting better fitting mathematical  
612 mass transfer models (Fulazzaky, 2011), or by determining the selectivity of functional groups (e.g.  
613 Boehm titration, inverse gas chromatography (IGC) (Fulazzaky et al., 2019). Finally, investigations  
614 into enhancing the circularity and economic and environmental sustainability of biosorption in  
615 practice via life cycle assessments (LCA), desorption, prior extraction of high-value compounds, or  
616 potential uses of the spent biosorbent material e.g. soil amendment (Pap et al., 2020).

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618

## 619 **4. Conclusions**

620 The main purpose of this study was to demonstrate that the pre-processing or production of algal  
621 biomass could have important implications upon the resultant biochemical and pollutant removal  
622 qualities of a biosorbent material. As such, the *C. parriaudii* biomass employed within this study was  
623 produced by cultivating with different nutrient regimes, designed to elicit varying biochemical  
624 profiles. Both the nitrogen type and the N:P ratio had an impact upon the final composition of the  
625 biomass, particularly in terms of the protein and carbohydrate content, which ranged from 8.5-  
626 13.6% and 32-44.2% DW, respectively. The material was then used for the adsorption of different  
627 metals, namely Al, Cu, Mn, and Pb, provided across a concentration range. Metal removal varied  
628 with metal type, initial concentration, and the nutrient regime in which the biomass produced with  
629 values of 0.023-1.636, 0.005-0.885, 0.005-0.658, and 0.002-0.855 mmol g<sup>-1</sup> DW recorded for Al, Cu,  
630 Mn, and Pb, respectively. FTIR analysis indicated that functional groups associated with proteins and  
631 polysaccharides play an important role in metal adsorption, while SEM-EDX indicated that elements  
632 including Ca, Fe, Mg, P, and Si are involved with adsorption. Since all other experimental factors  
633 were identical, the observed variation and means of metal removal between treatments (Figs 1-4 &  
634 Supplementary Table S1) can only be attributed to biological variability and cell surface properties  
635 induced by the cultivation under different types of media. Therefore, through a broad and robust  
636 methodology, the experimental hypotheses set out in this study have been proven: nutritional  
637 history, and putatively other biological aspects as an indirect extension of this, play a significant role  
638 in the biomass qualities produced and their subsequent usefulness for pollutant removal. Previously  
639 published studies of a similar nature will have overlooked this aspect making scientific  
640 reproducibility a challenge. Furthermore, this could explain the broad variation in metal removal  
641 values on an inter- and intra-species level previously reported. Since cultivation conditions have a  
642 considerable influence upon metal removal, much greater consideration should be granted to the  
643 conditions used to produce biosorbent material in future studies of this kind. Finally, understanding

644 the influence of biomass cultivation processes could have significant practical applications in terms  
645 of reproducibility, pollutant removal efficacy and consistency, and the cost of biosorbent materials  
646 produced.

647

## 648 **Supporting Information**

649 Figures and Tables relating to FTIR-ATR, SEM-BSE and EDX spectra are available.

650

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661

## 662 **Author Information**

663 M.E.R. and A.J.C.S. conceived and planned the project. M.E.R. conducted the experiments,  
664 generated, collated, and processed the data. M.E.R. and A.J.C.S. interpreted the results. M.E.R.  
665 wrote the manuscript. M.E.R., M.S.S., J.G.D., and A.J.C.S. reviewed and edited the manuscript.  
666 M.S.S., J.G.D., and A.J.C.S. supervised the project and acquired the funding.



667 **Author Information**

668 The authors declare that they have no competing interests.

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